Early Estimation of Gas Well Reserves Using BHP Buildup and Drawdown Data

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INTRODUCT ION

The need for early estimation of gas reserves on deep exploration wells has long been apparent. In an effort to evaluate techniques for early determination of gas reserves, extensive bottom hole pressure and production tests were recently run on 2 new completions. Test Well No. 1 is completed in the Pennsylvanian, and Test Well No. 2 is completed in a lower Permian formation.

Although the subject tests will not result in reliable quantitative reserve estimates in all cases, they should furnish a range of reserves valuable in making decisions concerning the timing of offset development. In addition, other useful data, relating to formation capacity and possible well bore damage, can be determined from the buildup tests. For larger reservoirs, these data can conceivably be of economic importance in indicating the need for and the anticipated results of additional stimulation.

RESERVE DETERMINATION METHODS EMPLOYED

In each test case, it was suspected beforehand that very limited reserves existed; consequently, it was estimated that steady-state flow conditions could be approached within 5 to 6 days. Under such conditions, the methods of determining well reserves as discussed below could be utilized. In addition, with sufficient total withdrawals during the test, a dependable material balance calculation provided a check on the other methods.

Park Jones¹ has presented methods of estimating reserves from gas well reservoir limit tests utilizing drawdown data where either transient or steady-state flow results. Where the test duration is insufficient for transients to effectively reach reservoir boundaries, a minimum reserve value can be established. In the subject tests, apparent steady-state flow was reached; however, data limitations permitted use of drawdown data for only Test Well No. 2. Park Jones's steadystate calculation is, in reality, a differential material balance type calculation as used herein.

Basically, 3 methods of computation have been employed in the subject tests as follows:

- 1. <u>Material Balance or P/Z Type Calculation</u> -<u>Necessitates a measurable decrease in static</u> reservoir pressure as a result of the total test withdrawals.
- 2. <u>Differential Material Balance</u> Necessitates a steady-state condition be reached during the drawdown test, or a linear relationship between flowing BHP and time at constant producing rate.

3. Integral Method² - Utilizes buildup curve data. Theoretically applicable only if steady-state conditions are reached during the flow test.

FIELD PROCEDURE

The field or test procedure consisted of the following:

- 1. Initial static reservoir pressures were determined after a substantial shut-in time. In the subject tests, both test wells had been shut-in in excess of 1 month awaiting pipeline connections.
- 2. The wells were placed on flow at near constant rate with a bottom hole pressure bomb down hole. The flow test (drawdown) was continued 5 to 6 days. A 180 hr. chart drive clock was used in the bomb during the drawdown test.
- 3. The wells were shut-in and bottom hole pressure buildups were recorded with both a 3 hr. chart drive and a 72 hr. chart drive.

As mentioned previously, the length of time on flow should be sufficient to allow steady-state conditions to prevail. The required time can be estimated from the following formula:

$$t = \frac{1.69 \, \emptyset \, \text{uc } r_e^2}{K} \tag{1}$$

Where: t = producing time, hours

 \emptyset = porosity, fraction

u = viscosity, cp.

re = drainage radius, feet

K = permeability, darcys c = fluid compressibility, psi⁻¹

RESULTS AND DISCUSSION

General data from the field tests are shown by Tables 1 and 2. Table 3 is a tabulation of results for each well and method of calculation. Step-by-step calculations are shown in the Appendix for Test Well No. 2.

TABLE 1 GENERAL DATA TEST WELL NO. 1

Drawdown Test Data:

| Gas Gravity | | 0.653 | |
|--------------------|----------------|---------------------|--|
| Distillate Gravity | | 55,1° API | |
| Total Time on Flow | | 140 Hours 5 Minutes | |
| Total Gas | High Pressure | 6,020 MCF | |
| | Low Pressure | 186 MCF | |
| Total Distillate | | 390 Bbls. | |
| Total Water | | 1 Bbl. | |
| Gas Rate | Maximum | 1,130 MCFPD | |
| | Minimum | 975 MC FPD | |
| | Average | 1,025 MCFPD | |
| | Final 24 Hours | 995 MC FPD | |

Pressure Data:

| Pressure Datum | 13,007 ft. |
|-----------------------|-----------------|
| Initial Static BHP | 5,499 psi |
| Drawdown Pressures | Erratic |
| Buildup Pressures | See Fig. 2 |
| Final Static BHP | 5044 psi |
| Reservoir Temperature | 180° F |

Miscellaneous Data:

| Casing | |
|--------|--|
| Tubing | |

Packer Setting Depth Perforations Formation Stimulation Calculated Absolute Open Flow

TABLE 2 GENERAL DATA TEST WELL NO. 2

5-1/2 in, set at 13,200 in 8-3/4 in, hole 2-7/8 in, to 13,011

(Open-ended)

Pennsylvanian

1420 MC FPD

500 Gallons Acid

12,973 ft. 13,004-13,010 ft.

Drawdown Test Data:

| Gas Gravit | y | 0.676 |
|--------------------|----------------|-------------|
| Distillate Gravity | | 65.4° API |
| Total Time on Flow | | 120 Hours |
| Total Gas | High Pressure | 17,494 MCF |
| | Low Pressure | 417 MCF |
| Total Distillate | | 1046 Bbls. |
| Total Wate | r | 44 Bbls. |
| Gas Rate | Maximum | 3619 MCFPE |
| | Minimim | 3242 MCFPL |
| | Average | 3499 MC FPE |
| | Final 24 Hours | 3300 MC FPL |

Pressure Data:

| Pressure Datum | 10,700 ft. |
|-----------------------|-----------------|
| Initial Static BHP | 4080 psi |
| Drawdown Pressures | See Fig. 1 |
| Buildup Pressures | See Fig. 3 |
| Final Static BHP | 3368 psi |
| Reservoir Temperature | 150° F |

Miscellaneous Data:

Casing

| Tubing | |
|------------|--|
| T dovening | |

Packer Setting Depth Perforations Formation Stimulation Calculated Absolute Open Flow 5-1/2 in. set at 13,000 ft. in 6-5/8 in. hole 2-7/8 in. to 10,600 ft. (Open-ended) 10,600 ft. 10,690-10,710 ft. Lower Permian 200 Gallons Acid

10 MMC FPD

| | TABI | LE 3 | |
|-------------------------------------|---|---|--|
| Method | <u>RESERVE S</u> Initial Gas- in-Place MMCF | Ult. Gas Reserves, MMCF | Estimated Ult. Distillate, Bbls. |
| | TEST WE | LL NO. 1 | · |
| Madamial Dalawa | | | |
| Material Balanc | 120 | 196 | = 700 |
| Using Z | 154 | 140 | 6 400 |
| Using Z | 104 | 140 | 0,400 |
| Differential Material Balance | Drawdown flow rate (| curve errati low capacity) | c due to low |
| Dalanee | | | |
| Integral | | | |
| $r_{o} = 100^{\circ}$ | 143 | 130 | 5,900 |
| 1000' | 199 | 182 | 8,300 |
| 2640' | 220 | 200 | 9,100 |
| | TEST WE | LL NO. 2 | |
| Material Balanc | e | | |
| Using C | 145 | 129 | 5.400 |
| Using Z | 155 | 138 | 5,800 |
| Differential Material Balar | 179 nce | 160 | 6,700 |
| Integral | | | |
| r - 100' | 208 | 185 | 7 800 |
| ^{-e} ⁻ 1000' | 291 | 260 | 10,900 |
| 2640' | 324 | 288 | 12.200 |
| | $\begin{tabular}{lllllllllllllllllllllllllllllllllll$ | $\begin{tabular}{ c c c c } \hline TABI \\ \hline RESERVE S \\ \hline Initial Gas- \\ in-Place \\ MMCF \\ \hline \hline Method \\ \hline \hline TEST WE \\ \hline \end{tabular} \\ \hline \end$ | $\begin{array}{c c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} TABLE \ 3 \\ \hline RESERVE \ SUMMARY \\ Initial \ Gas- & Ult, \ Gas \\ in-Place & Reserves, \\ MMC \ F & MMC \ F \\ \end{array} \end{array} \\ \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \begin{array}{c} \end{array} \end{array} \\ \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \\ \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \\ \end{array} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \\ \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \\ \begin{array}{c} \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \\ \end{array} \end{array} \\ \end{array} \\ \end{array} \\ \end{array} \end{array} \end{array} \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \end{array} \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \\ \end{array} \end{array} \\ \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \\ \end{array} \end{array} \\ \end{array} \end{array} \\ \end{array} \end{array} \end{array} \end{array} \\ \end{array} \end{array} \end{array} \end{array} \\ \end{array} \\ \end{array} \end{array} \\ \end{array} \end{array} \\ \end{array} \\ \end{array} \end{array} \\ \end{array} \end{array} \\ \end{array} \end{array} \\ \end{array} \\ \end{array} \end{array} \\ \end{array} \\ \end{array} \\ \end{array} \\ \end{array} \\ \end{array} \\ \end{array} \end{array} \\ \end{array} \end{array} \\ \\ \end{array} \\ \end{array} \\ \end{array} \\ \\ \\ \end{array} \\ \\ \\ \end{array} \\ \\ \\ \\ \end{array} \\ \\ \\ \end{array} \\ \\ \\ \\ \\ \end{array} \\$ |

Material Balance Method

In each of the subject tests, the reserves were of such low magnitude that appreciable decreases were observed in the static reservoir pressures as a result of the test withdrawals. This condition resulted in reliable material balance estimates of reserves by either of the following formulae:

$$G = \frac{W_d}{5.61 B_g C\Delta} P_s$$
(2)

$$G = \frac{5.03 \text{ g T}}{B_{g}} \frac{1}{(P_{si}/Z_{i} - P_{sf}/Z_{f})}$$
(3)

- = gas volume factor, Bbls/MCF
- Bg C = average fluid compressibility, psi-1
- = reservoir withdrawals at standard g conditions, MCF
- т = reservoir absolute temperature, °R
- $P_{si}P_{sf}$ = initial and final static pressure, psia
- $Z_i, Z_f =$ initial and final gas compressibility factor.

Equation (3) is the more accurate in that it does not involve the average compressibility term, which term introduces error since it is a non-linear function of pressure. Equation (3) is the equation of the straightline plot of P/Z versus cumulative recovery normally utilized in graphically determining gas reserves and will yield identical results as the plot extrapolated to zero gage pressure.

The initial gas-in-place for Test Wells No. 1 and 2 was 155 MMCF and 154 MMCF, respectively, by material balance calculation. The similarity in the numbers is coincidental.

The material balance method is expected to be the most accurate of the methods employed in analyzing these tests; however, it is pertinent to point out that this method is not applicable to reservoirs where the total withdrawals during the test are not of sufficient

quantity to create a measureable difference in the initial and final static pressures. In addition, the shut-in times must be sufficient to give reliable static pressures by extrapolation. Obviously, the closer the initial and final pressures the more chance for percentage error due to bomb limitations and shut-in extrapolation.

Differential Material Balance or Drawdown Test Method

This method is a solution of the material balance equation differentiated with respect to time, or a solution of

$$G = Q$$

$$C dp/dt (4)$$
Where: G = gas-in-place, MCF
$$Q = withdrawal rate, MCF/day$$

$$C = average compressibility, psi-1$$

$$dp/dt = slope of pressure versus time$$

$$curve, psi/day$$

For application of this method, the flowing bottom hole pressure must reach an approximate linear relationship with time. Such was the case for Test Well No. 2. as shown by Fig. 1. This relationship was not apparent for Test Well No. 1 due to erratic flowing bottom hole pressures believed attributable to the relatively low rate of 1000 MCF per day (low capacity) resulting in apparent liquid accumulation and unloading in the tubing during the test.



The differential material balance yielded a gasin-place of 179 MMCF for Test Well No. 2 as compared to 155 MMCF by conventional material balance calculations.

This method is identical to that presented by Park Jones¹ for steady-state or bounded reservoir conditions.

Integral Method

The integral method involves solution of the following equation: Θ = ∞

$$V_{p} = \frac{0.829 \times 10^{-3} \text{ kh}}{F \text{ u c}} \int \frac{(P_{s}^{2} - P_{w}^{2}) \text{ dQ}}{(P_{s}^{2} - P_{o}^{2})}$$
(5)

Where: ^Vp = gas pore volume, cu. ft. kh = interwell capacity, md-ft

- P_S = final static pressure, psi
- P_W = shut-in bottom hole pressure, psi
- $P_0 =$ final flowing BHP, psi
- ο = build-up time
- F = function of drainage and well radii, dimensionless
- u, c = as previously defined

Numerical values for each of the above terms are available from the drawdown and buildup test data, except for the function F. For non-fractured systems, such as the subject cases,

$$\mathbf{F} \stackrel{\frown}{=} \frac{1}{4 \ln r_{\rm e}/r_{\rm W}} \tag{6}$$

It is necessary to assign values to the drainage radius, re, and the effective well bore radius, rw, for use in the integral method. Since these values appear as a log function, they are not seriously critical in a non-fractured system, as shown by the tabulation of results, Table 3. The results of the integral method are shown on this tabulation to be higher than, but comparable with, the previously discussed reserve calculations

The integral method has a number of limitations, primarily related to the necessity of reaching steadystate flow during the drawdown test. In cases where the integral method is applicable, the first 2 methods might also be applicable; however, in situations such as with Test Well No. 1, where 1 of the first methods fails, 2 methods remain for comparison.



Test Results

Table 3 is a tabulation of results for each well and method of calculation. Ultimate gas reserves as reflected in this table are those reserves recoverable to an abandonment pressure of 500 psia. The reserves of each of the test wells are extremely low, being in the order of 150 to 200 MMCF, certainly far below those reserves required for additional development. By comparing the ultimate gas reserves as calculated by the various methods, it is apparent that reasonable agreement was achieved between the methods.

In reporting results of the integral method, 3 values of drainage radius are shown with ultimate gas reserves calculated for drainage radii of 100 ft., 1000 ft. and 2640 ft., with the ultimate gas reserves ranging from 185 MMCF to 288 MMCF, a less than 2 fold increase for a 26-fold increase in the value of drainage radius. It is not recommended that drainage radius be determined by comparing reserves calculated by the integral method to reserves calculated by other methods.

Actual Performance As Verification of Test Results

Actual performance of the 2 test wells in the form of bottom hole pressure versus cumulative production is shown by Fig. 4. Extrapolation of the pressure performance of Test Well No. 1 indicates an ultimate gas recovery of 148 MMCF to an abandonment pressure of 500 psia. After producing approximately 80 MMCF from this well, additional intervals were perforated in the formation not in communication with the initial zones perforated.

An extrapolation of BHP/z versus cumulative gas recovery for Test Well No. 2 indicates an ultimate recovery of 124 MMCF to an abandonment pressure of 500 psia. For both test wells, subsequent performance has verified the range of results obtained from the initial pressure and production tests.

As a matter of interest, the pore volume reserves as calculated from log derived parameters exceeded 4 billion cu. ft. for each of these wells based on drainage areas of 640 acres, resulting in favorable offset economics in the absence of the pressure and production tests or subsequent producing performance.

A third test similar to those reported herein was run on another Pennsylvanian gas well; however, equipment failures after approximately 22 hr. on flow required discontinuation of the test. Nevertheless, the data obtained were utilized in calculations to arrive at an estimate of the ultimate gas reserves. The results of the test data indicated reserves of approximately 900



MMCF. Subsequent pressure-cumulative data on this well, extrapolated to an abandonment pressure of 500 psi, indicate an ultimate recovery of 650 MMCF.

Conclusion

In limited reservoirs, early pressure-production testing can be valuable in efforts to postpone decisions concerning offset development until sufficient performance data are obtained to verify the test results.

APPROXIMATE COST OF TEST

The subject tests required approximately 9 days of field testing, Depending on the location of the well, considerable engineering time or field personnel time can be involved. In addition, 1 or 2 days of engineering office time are required to accumulate data and make the necessary calculations. Wire line service costs and equipment rental charges for each test are approximately \$250, exclusive of the bottom hole pressure bomb. An Amerada Type RPG-3 bomb was used on all surveys.

ACKNOWLEDGEMENT

Appreciation is expressed to Pan American Petroleum Corporation for permission to present these tests and results, and to engineering and production personnel contributing to these tests, particularly Mr. Ed Snook, who gathered most of the field data and aided with interpretation.

REFERENCES

- 1. Park Jones, "Reservoir Limit Test on Gas Wells". Journal of Petroleum Technology, p. 613, June, 1962.
- Scott, P. H.: "An Integral Method For Determining Reservoir Pore Volume From Pressure Buildup Data", Private Communication from Pan American Petroleum Corporation Research Department.

APPENDIX

RESERVE CALCULATIONS TEST WELL NO. 2

I. Material Balance:

 $P_{si} = 4080 \text{ psi}$ 3368 psi р

The final static pressure was chosen as an approximate average on Part III of the buildup curve, Fig. 3. The deviation of all points adjacent to the horizontal line is less than 8 psi which is within the accuracy of the bomb and interpretation; therefore, it is believed that the pressure had stabilized at an average value.

Using Equation (2): (Compressibility)

$$G = \frac{W_{d} (2)}{5.61 \text{ Bg C } \Delta P_{g}}$$

$$B_{g} = 5.04 \frac{Tz}{P} \frac{\text{bbls}}{\text{MCF}} = \frac{5.04 (610) 0.869}{4080}$$

$$B_{g} = 0.653 \frac{\text{bbls}}{\text{MCF}}$$

$$C = \frac{1}{P} - \frac{1}{z} \frac{dz}{dp} \qquad P_{ave} = 3724$$

$$C = \frac{1}{3724} - \frac{1}{.84} (78 \times 10^{-6}) = 176 \times 10^{-6} \text{ per psi}$$

dz/dp is the slope of pressure versus z at the average pressure.

 $\begin{array}{l} W_{\rm d} = 17,911 \ \text{x} .653 \ \text{x} \ 5.61 = 65,700 \ \text{cu. ft.} \\ \Delta P_{\rm s}^{\rm d} = 4080 \ - \ 3368 \ - \ 712 \end{array}$

$$G = \frac{65,700}{5.61(.653) 176(712)} 10^6 = 145 \text{ MMSCF}$$

At an abandonment pressure of Pa, the ultimate gas recovery is given by the following:

Ult. Gas = G(1-0.1985
$$\frac{P_a B_{gi}}{Z_a T}$$

= 145 $\begin{bmatrix} 1-0.1985 & 500(.653) \\ & .93(610) \end{bmatrix}$
= 145 (.89)

Ult. Gas = 129 MMCF @ Pa = 500 psi

Using Equation (3): (Compressibility Factor)

$$G = \frac{5.03 \text{ g T}}{B \text{ g}} \left(\frac{1}{P_{\text{si}}/Z_{\text{i}}} - \frac{1}{P_{\text{sf}}/Z_{\text{f}}} \right)$$

$$G = \frac{5.03 (17,911)(610)}{.653} \left(\frac{(1)}{.869} - \frac{3368}{.812} \right)$$

$$G = 155 \text{ MMC F}$$

Ultimate Gas Recovery = 155 x .89 = 138 MMCF

A P/Z versus cumulative plot yields the same values.

II. Differential Material Balance:

Using Equation (4)

$$G = \frac{Q}{C dp/dt}$$

The near straight line portion of Fig. 1 yields a slope of 4.35 psi/hr. therefore.

$$G = \frac{3300}{176 \times 4.35 \times 24}$$

G = 179 MMCF

III, Integral Method:

The integral method pore volume is expressed by Equation (5) $\mathbf{O} = \infty$

$$V_{\rm p} = \frac{0.829 \times 10^{-3} \text{ kh}}{F \text{ u c}} \int \frac{({\rm P_s}^2 - {\rm P_w}^2)}{({\rm P_s}^2 - {\rm P_o}^2)} \frac{d\Theta}{\Theta}$$

The value of the integral, 0.845, was determined by planimetering the area under a plot of ($P_s^2 - P_w^2$) versus Q.

The capacity, kh, is determined by

 $kh = \frac{1637 \text{ QuTz}}{m}$

where m is the slope in psi 2/cycle of the interwell, Part II, portion of the buildup curve shown on Figure 3. m = 0.356 x 10^6 psi2/cycle.

Insert Figure 3

Gas viscosity can be estimated from various handbooks, expressed as a function of temperature, pressure and gravity. As discussed previously, the F function for unfractured well systems is approximately

$$F = \frac{1}{4 \ln r_e/r_w}$$

Therefore,

$$V_{p} = \underbrace{0.829 \times 10^{-3} (201)}_{F(.025)(176 \times 10^{-6})} \underbrace{0.845}_{0.845}$$

$$V_{p} = 32,000/F$$

For various values of re

| r_{e} | \mathbf{F} | vp | G | Ult. Reserves | |
|---------|--------------|-----------|-----|---------------|---|
| | _ | <u> </u> | | | • |
| 100' | .042 | 762,000 | 208 | 185 | |
| 1000' | .030 | 1,067,000 | 291 | 260 | |
| 2640' | .027 | 1,185,000 | 324 | 288 | |
| | | | | MMSCF | |

Where

$$G = \frac{Vp}{5.615 \times B_{cr}} = \frac{Vp}{3.66}$$

Ult. Gas Reserves = 0.89 G for $P_a = 500$ psi.



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