

# PRODUCTION CHEMICAL APPLICATIONS: USING ANALYTICAL DATA TO MONITOR AND OPTIMIZE CHEMICAL TREATMENTS

Becky L. Ogden  
Multi-Chem—A Halliburton Service

## ABSTRACT

Advancing technology has enabled the oil and gas industry to analyze and track constituents in fluid samples. However, without proper sampling, appropriate laboratory procedures, and correct interpretations of such analyses, these data could be erroneous and result in costly and unnecessary actions. Through proper analytical sampling, testing, and understanding of these results, operators can monitor and optimize chemical applications.

This paper discusses the following:

- Common analytical testing performed within the oil and gas production chemical industry
- Identification of critical hold-points within these procedures
- Common general rules for the identification of possible anomalies during such analyses
- How these tests can be applied to assist optimization of chemical applications

Key Words: analytical, anomalies, interpretation, results, optimization, chemical applications

## INTRODUCTION

Within the oil and gas industry, well fluids are sampled and analyzed for a variety of purposes, ranging from general knowledge analyses to determining the economic viability of a well or field. Considerable costs can be associated with well treatments based on data incorrectly interpreted or fluids incorrectly sampled or handled. Such treatments might not have been necessary. Ensuring proper handling of samples and correct interpretation of the results helps provide confidence in the analytical testing results and the application of these results during the chemical treatment of a well.

Chemicals can help minimize disruptions during the lifecycle of a well, reduce well or pipeline corrosion rates, enhance oil and water separation, reduce the amount of solids in wellbore fluids, and control micro-organisms. While these are examples of the many positive economic attributes provided, chemicals can also impact the safety and environmental performance of treatments. Analytical tests can be performed to support and optimize chemical treatments to help reduce or eliminate these concerns (Ogden, 2006).

The analytical tests most commonly conducted for oilfield chemical support include water analyses, product residuals (scale, corrosion inhibitors), total filterable solids, corrosion coupon analyses, bacterial enumeration tests, solids analyses, and oil and grease analyses. Each of these tests has a specific and unique set of detail, sampling, and preservation needs; additionally, understanding the results of these tests is crucial to designing an appropriate and effective chemical program.

## SAMPLING AND MONITORING

Understanding the characteristics of the producing fluids from a well can assist with identifying current or future operational challenges. Screening production chemicals with those fluids can help identify the appropriate chemical additive to address those challenges; however, to optimize a well's chemical treatment, the response to that chemical additive should be determined. Through effective monitoring, tracking, and trending of analytical data, it is possible to determine whether the well responds favorably or if modifications to the treatment should be implemented.

When determining the specific analyses necessary, it is important to know the following:

- Properties being measured

- Test purpose
- Sample amount to be collected
- Possible contaminants that could adversely affect results
- Industry standards for sampling, preserving, and conducting the analytical test
- Allowable sample-to-analysis timeframe

#### IDENTIFICATION OF CHEMICAL-RELATED PRODUCTION CHALLENGES

As fluids flow from the wellbore into the various surface vessels and tanks, the operating conditions within these locations change (Patton, 1986). As these changes occur, production challenges can be impacted. It is important to acknowledge that, while certain challenges can be present in the downhole environment, they might be somewhat different, or even non-existent, in the surface equipment. Velocity, pressure, pressure reduction, and temperature can vary greatly as fluids progress through the production system. Additional analytical testing might be necessary to determine the magnitude of these challenges at each location in the system. Table 1 identifies common challenges throughout a production system and the associated analytical tests. Sampling upstream and downstream of production equipment can be helpful in terms of determining the severity of a production challenge following a modification in the operational parameters (pressure/temperature).

After completion of product screening and implementation of the resulting recommendations, it is imperative to monitor and track the response from the well or piece of equipment. Without proper monitoring, it is difficult to assess the success of the chemical application. The following sections identify common analytical techniques and discuss their application for optimizing chemical treatment.

#### ANALYTICAL TESTS ASSOCIATED WITH CHALLENGES

##### Water Analyses

Water is often referred to as the universal solvent; as such, it dissolves and carries many impurities (Patton, 1986). These impurities can be troublesome within many industries, including the oil and gas industry. While water is viewed as a byproduct of production in the oil and gas industry, it can contain vital information about reservoir characteristics, corrosiveness in a well, the tendency for mineral scale deposition, and many other factors pertaining to oil and gas production. Without water, many of the production challenges experienced in the oil and gas industry would be substantially minimized.

Water analysis is one of the basic analytic tests performed by the oil and gas industry; however, results are frequently misunderstood and misapplied. Table 2 shows the primary components of water analysis (Martin, 1965). Depending on the final use of the water being analyzed, additional components, such as boron or silica, can be added to the analysis; however, this table details the most commonly identified components observed in oil and gas produced water.

When proper sampling, preservation, and analytical procedures are used, the analyst or engineer can interpret the water analysis with confidence. By analyzing for the constituents listed in Table 2, several conclusions can be ascertained.

##### *Uses for Water Analyses: Identification of Production Zones*

Production zones have distinct water properties characteristic to the location within a given county or geographic area (Martin, 1964). These records have been gathered, cataloged, and used for more than 50 years by independent laboratories to aid identification of production zones or contamination within a production zone (Martin, 1965). The characteristics are highly dependent on chlorides, calcium, magnesium, sulfate, barium, and the ratios of these cations and anions to each other. It is recommended to conduct a water analysis as soon as possible after a well has stabilized following its initial completion, recompletion, or when new zones are opened for production. When suspect production trends are noted, a repeat water sample can be captured and analyzed. An accurate water analysis can be compared to existing historical records for a specific well or on offset well records within the geographic area to determine if the produced water is characteristic of the water produced from that formation or if possible casing leaks, foreign water entry, or contamination have occurred (Patton, 1986). An accurate water analysis is vitally important in such situations because costly well workovers could be scheduled based

on the results. It is recommended to conduct a repeat water analysis before rigging up on a well to verify the suspect water constituent values.

#### *Predicting Corrosivity*

Water analysis can indicate whether corrosion is likely to occur based on several factors (Van Delinder, 1984). Water analysis identifies acid gases in the produced water as well as the dissolved minerals and metals that could contribute to the corrosion process. For accuracy, acid gases ( $\text{CO}_2$  and  $\text{H}_2\text{S}$ ) should be tested on location immediately after the sample is obtained (API RP-45, 1998). The acid gas content determines the dominate type of corrosion and significantly influences the corrosion rate of a system. Corrosion rates are directly related to the amount of such gases dissolved in the produced water in combination with the dissolved chlorides and system pressures.  $\text{CO}_2$  corrosion can result in various forms of metal loss and pitting.  $\text{H}_2\text{S}$  can result in a severe pitting attack and can often create high pitting/failure rates. In systems where  $\text{CO}_2$  and  $\text{H}_2\text{S}$  are both produced, the ratio of  $\text{CO}_2$  to  $\text{H}_2\text{S}$  determines which species dominates corrosion in the system.

When  $\text{CO}_2$  and  $\text{H}_2\text{S}$  dissolve in water, they form acids. As the levels of dissolved  $\text{CO}_2$  and  $\text{H}_2\text{S}$  increase in the water, the pH of the produced fluids declines. This creates a corrosive environment. Dissolved  $\text{CO}_2$  or  $\text{H}_2\text{S}$  present in the water, when combined with the low pH and high chloride content, is indicative that the water is potentially corrosive in nature. As with acid gases, the pH of the water should be tested on location immediately after the sample is obtained.

In addition to reviewing the acid gases, chloride levels, and pH, it is also advantageous to review the levels of iron and manganese contained within the water sample. Because these are analyzed on acidized samples, the measurements are reflective of both dissolved and any suspended compounds that were solubilized by the acid, referred to as "total iron and total manganese." High iron and manganese levels can be indicative of active corrosion occurring downhole or in surface equipment. Additional monitoring of equipment integrity, reviews of failure records, and visual inspection of any removed metallic components are recommended to verify active corrosion. Depending on their history, older waterfloods can sometimes recirculate iron and manganese, making interpretation during the monitoring process difficult. In such situations, it is recommended to review trend analyses on iron/manganese and attempt to relate these trends to actual field corrosion failure data.

In some instances, water analyses can include a determination for oxygen. This is commonly included for water injection or water disposal systems and should be performed onsite for accuracy (Patton, 1990). Levels of oxygen should not exceed 50 ppb (0.050 ppm) when  $\text{H}_2\text{S}$  and/or  $\text{CO}_2$  are present. Not only is oxygen a severely corrosive species, but acid gas corrosion is accelerated in the presence of oxygen. In the absence of  $\text{H}_2\text{S}$  and/or  $\text{CO}_2$ , it is recommended for oxygen levels to be maintained below 100 ppb (0.10 ppm). Ideally, oxygen should be excluded or scavenged from production facilities.

Using water analysis to understand the potential for corrosion and relating this information to actual failure records for a field or area enables the producer to design an appropriate corrosion mitigation program. This program can consist of engineering solutions to remove the corrosive species, selection of corrosion-resistant alloys, application of protective coatings, or application of corrosion inhibitors.

#### *Predicting Scaling Tendencies*

Mineral scales are defined as mineral depositions that result from an oversaturation of a given compound in a solution under a certain set of conditions. Scales can result in plugging problems in the producing formation, downhole equipment, and/or surface piping/equipment. Additionally, under-deposit corrosion can occur beneath scale depositions, resulting in high corrosion rates and premature failure of production or pipeline equipment. Predicting the scale deposition tendency in water is achieved through the analysis and arithmetical combination of the cations, anions, pH, temperature, and pressure of the water and then comparing the saturation of the water to solubility constants under the temperatures and pressures noted (Oddo and Tomson, 1994). A pressure drop can indicate the potential for calcium carbonate ( $\text{CaCO}_3$ ) scale formation. Increased temperatures (i.e., submersible pumps or surface pumps) can result in a potential for calcium sulfate ( $\text{CaSO}_4$ ) scale formation. Barium sulfate ( $\text{BaSO}_4$ ) scale, which is insoluble in water, forms upon mixing of incompatible waters.

These calculated tendencies are only indicators of possible deposition that might occur given the operating conditions of the system, including pressure reductions and temperatures of the produced fluids. It should be noted that calcium carbonate mineral scales have an inverse solubility in water as the temperature increases (i.e., they become less soluble as temperatures increase). The solubility of calcium sulfate scales increases up to a temperature of 50°C but then decreases with increasing temperature, and the solubility of barium sulfate scales increases with increasing temperatures (Figure 1). Therefore, as temperatures change, the likelihood of scale deposition can vary.

Typically, three (3) types of mineral scales are present in production and injection systems: calcium carbonate, calcium sulfate, and barium sulfate. Table 3 shows the solubilities of these scales in water (calcium sulfate > calcium carbonate > barium sulfate). Table 4 shows the primary variables that can result in the deposition of these mineral scales.

**Calcium Carbonate** scale (Figure 2) is an acid-soluble mineral scale that forms easily and is most common in low-pressure systems and injection wells. This scale deposition can be removed with the application of acid. However, acids will not typically penetrate an oil-wet solid; therefore, using a mutual solvent is necessary to assist removing the hydrocarbons from the scale. This allows the acid to effectively dissolve the mineral scale and clean the equipment. Calcium carbonate scale can be prevented and controlled using low concentrations of scale inhibitor.

**Calcium Sulfate** scale (Figure 3) is the second most common scale observed in production/water systems and is formed through pressure and temperature variances. This scale is not acid-soluble and must first be chemically converted to an acid-soluble salt using a sulfate converter or removed using a specialized dissolver. If a converter is used, a two-step procedure is necessary. The converter is applied to the system; the well (or equipment) is shut-in and allowed to react with the calcium sulfate scale. This shut-in time is generally 12 to 24 hours. Once the sulfate scale has been converted to an acid-soluble form, acid can be applied to remove the converted mineral deposition.

It is possible to use a calcium sulfate dissolver in some applications to reduce the two-phase cleanup to a single application. The product is designed to dissolve calcium sulfate molecules in a single procedure. It is not necessary to apply acid in conjunction with this application. However, it is recommended to allow at least 12 to 24 hours for the process to completely dissolve the scale present.

**Barium Sulfate** scale (Figure 4) is the third mineral scale that can be present in production/water systems. This scale is neither acid-soluble nor can it be dissolved economically. Once this scale is formed, it is usually removed by mechanical methods. Barium sulfate scale will form before calcium sulfate scale if there is any barium present in the produced water with any amount of sulfates. This type of mineral scale can be inhibited, but a higher chemical concentration is usually necessary to be effective.

Other types of depositions can occur; however, many are byproducts of bacterial activity and acid gas corrosion of metallic components or the result of mixing incompatible waters. Reviewing the water analysis and field failure history and monitoring for biological activity can help determine the origin of deposits. Iron carbonate and iron sulfide are two deposits that can originate from either corrosion or biological activity. They are generally not categorized as scales but as “deposits” and are most effectively controlled using corrosion inhibitors and biocides or by controlling the quality of makeup water for injection systems (i.e., mixture of incompatible waters).

#### *Understanding Chemical Solubilities*

A water analysis is also helpful for understanding the solubilities of production chemical products. Knowledge of the chloride level is crucial for the selection of gas enhancement products (i.e., foam-assisted lift products). The total dissolved solids (TDS) content and calcium levels in a water are also important factors for the solubility of scale and corrosion inhibitors. Again, an accurate water analysis is the beginning for screening such products and is necessary to design an effective program to address production challenges.

### *Recognition of Possible Anomalies in Water Analyses*

When reviewing a water analysis, a few general rules can assist in determining the presence of possible anomalies (Ogden, 2008). Comparing current analyses with historical analyses is important to help identify possible changes in the water composition or possible anomalies for follow-up confirmation. General guidelines include the following:

- Compare the measured density of the water to the TDS to determine if errors exist in the reported figures.
- Compare reported sulfate values to reported barium values. Unless scale inhibition is present (and effective), barium content should be relatively low (2 to 3 mg/L) if sulfate values are at, or exceed, 150 to 200 mg/L in the water.
- Compare the ratio of total iron to total manganese; if the source of the manganese is the result of carbon steel alloy corrosion, it should be 1 to 1.5% of the iron levels.
- Check the alkalinity, pH, and CO<sub>2</sub> levels. At a pH equal to or less than 4.5, only CO<sub>2</sub> is present; at pH levels greater than 4.5 but less than 8.3, CO<sub>2</sub> and bicarbonate (HCO<sub>3</sub><sup>-</sup>) will be present; at pH levels above 8.3 but less than 10.2, bicarbonates (HCO<sub>3</sub><sup>-</sup>) and carbonates (CO<sub>3</sub><sup>-2</sup>) will be present, but no CO<sub>2</sub> will be present. At pH levels greater than 10.2, carbonates and hydroxyl (OH<sup>-</sup>) will be present.
- If the water pH is low (below 6) but alkalinity is high, additional analytical work might be justified. Organic acids might be present (these are a part of the water alkalinity).
- The fresher the water (low TDS), the more oxygen a water can contain. Fresh water (TDS less than 1000 mg/L) is saturated with oxygen (at room temperature, atmospheric pressures)—between 6 to 8 ppm oxygen.
- Oxygen readings need to be performed in the field to ensure accuracy. Unusually high oxygen levels in a water sample can be indicative of a poor sampling technique (i.e., allowing the introduction of oxygen into the glass test ampule) or not conducting the oxygen determination in the field. Resampling and retesting onsite is recommended.
- Lower-pH water (less than 7.0) indicates the water could be corrosive (acidic).
- Higher-pH water (greater than 7.0) can indicate the water has increased scaling tendencies (especially with calcium carbonate scale).
- The higher the chlorides/TDS, the higher the potential for corrosion.
- Higher temperatures can indicate a greater potential for corrosion and/or scale.
- If unstable constituents were not determined onsite, erroneous scaling and/or corrosion tendencies are likely.
- If the water was not sampled in the appropriate container, or preserved correctly, erroneous data are likely. Refer to API RP-45 (1998) for details about containers and preservation techniques.
- If the sample valve was not adequately flushed before capturing the sample, impurities from the valve could be introduced into the sample container and solubilized upon acidification, altering the dissolved components reported during testing.

A water analysis can provide extremely informative analytical information and is integral to production chemical selection and monitoring, and it can aid in the design and development of secondary and tertiary recovery systems for the oil and gas industry. However, to provide these benefits, the water analysis must be correctly sampled, preserved, analyzed, and interpreted. Furthermore, it should be representative of the system being tested. Regular testing of produced waters (annually, unless conditions warrant a retest) can indicate whether corrective actions are necessary and will also assist with confirming the success, or failure, of past actions. The frequency of sampling should be modified if changes are implemented to a system or if conditions within a system deteriorate.

#### Total Filterable Solids

In addition to the TDS identified in the water analysis, understanding the total suspended solids (TSS) can be beneficial, particularly in a water injection or water disposal system. TSS are generally measured, examined, and analyzed using a membrane filter. NACE TM0173-2015 (2015) uses a preweighed 0.45-micron pore size filter pad. The water is filtered at 20 psig (delta pressure across the membrane filter) for up to 10 minutes or until a set volume of water has been filtered. The filter pad is then dried and reweighed

to determine the TSS. Further analyses can be conducted on the solids captured on the filter pad to yield useful information, such as hydrocarbon content, acid solubles, acid insolubles, and deposited particle sizes. TSS can be naturally occurring (silicates, sands) or can be formed as a result of corrosion by-products or mineral scale deposition. In terms of injection systems, a target TSS of 50 mg/L or less is desirable (Ostroff, 1979; Patton, 1990); however, if the matrix into which the water is to be injected is tight (i.e., low porosity and/or low permeability), knowing the particle sizes can be as important as the quantity of particles present. Both size and quantity of particles can be determined on the membrane filter.

TSS can result in solids deposition throughout a reservoir, on downhole equipment, or within surface equipment. TSS can also result in erosional damage to equipment, erosion/corrosion damage (especially with stainless steels), plugging of the reservoir or production equipment, and injectivity losses or reductions in injection wells, and it can be involved in the development of oil-field emulsions (normal and reverse emulsions).

Suspended solids can be addressed chemically and/or mechanically (Kemmer, 1979). Chemicals can aid in water-wetting solids and can be used in conjunction with mechanical solids removal equipment, such as WEMCO® units, upflow or downflow filtration units, hydrocyclones, and simple cartridge filtration. Solids removal should help increase the life expectancy of projects and equipment and increase the economics of such projects.

#### *Recognition of Possible Anomalies in TSS Analyses*

Tracking and trending the analyzed components present on the membrane filter can aid in the recognition of possible anomalies within the analysis or can expose possible upsets in the system. When a spike, or sudden decrease, in a value appears that is not statistically average for that sampling point, it is recommended to retest the location. It is imperative that the analyst in the field adequately purge the sample valve to help prevent the accumulation of “valve solids” on the membrane filter, which can result in an erroneously high TSS calculation during laboratory analysis. Additionally, oxygen should be purged from the sample line to help prevent ineffective filtration, which can result in an erroneously low TSS value during laboratory analysis of the filter.

Handling the membrane filter correctly is crucial for proper interpretation of the test. The filter must not be handled with bare hands (finger prints and oils from the skin can add weight and/or result in blocking the pores on the membrane), and the membrane must not be damaged in any way before, during, or after the field filtration test or during the laboratory analysis process. The filter is a preweighed, delicate membrane, and TSS calculation is based on the weight gained as a result of water being filtered through the membrane.

A common error in membrane filter analysis is omitting the initial distilled water rinse (before any acid washes), which removes water-soluble salts present on the membrane. When determining carbonate deposits, this results in a false elevation of carbonates after the first acetic acid rinse (followed by its subsequent distilled water rinse).

Again, understanding the water analysis can assist in predicting the types and possible location for the formation of suspended solids throughout a production facility (Ostroff, 1979).

Table 5 illustrates the common suspended solids and their probable origins. It should be noted that 1 mg/L of suspended solids equates to 0.00035 lbm/bbl of potential deposition. For a 10,000 BWPD injection system at 50 mg/L, depositing all TSS would equate to 175 lbm/day of solids or 32 tons of deposition per year.

#### *Solids Analyses*

The deposition of solids has long been recognized as a major economic concern. With increased concerns about improving the productivity of oil and gas operations, the continuing depletion of reservoirs, and the institution of waterflooding, pressure maintenance, and even more sophisticated recovery practices, the effects of solids deposition within the oil and gas industry is becoming increasingly significant. Effects, such as plugging of tubular goods used in lifting and handling petroleum, reservoir

damage, accelerated boiler or fire-tube failures, among others, can impair productivity in oil and gas recovery operations. Deposits can result in costly maintenance, remedial work, and equipment replacement.

While water analysis can model the likelihood for scale formation, solids analysis validates the system's actual tendency. Using solids analysis is important for understanding the types of deposits present within the production system. By determining the composition of the solids, it is possible to design a program for managing them.

As stated, mineral scales are defined as deposits that result from the oversaturation of a mineral in a solution. For oil and gas production, carbonate or sulfate deposits are most common. If the solids analysis indicates deposits are mineral scale, then management programs can be designed to address the formation of these scales. Analyses on deposits are important for the development of a removal and prevention program. Not only do they validate the scale prediction models of the water analysis, they yield information useful during the selection of the proper scale product. Scale removers and inhibitors are scale-type specific; certain inhibitor chemistries are better at inhibiting carbonate scales, while some are better at inhibiting sulfate scales. Additionally, it is important to identify the type of deposit before recommending a removal process. Table 6 lists common scales and their solubility with respect to water and acid.

An initial solids analysis can be performed relatively easily in the field using an organic solvent, water, and 15% hydrochloric (HCl) acid. By observing the reactions in each step, preliminary conclusions concerning the components of the solid can be quickly determined. Following this initial test, a more detailed analysis can be performed in the laboratory using wet-chemistry or instrumental analyses.

#### *Recognition of Possible Anomalies in Solids Analyses*

One common error with solids analyses often originates with the process used. For wet-chemistry methods, it is important to ensure all organics/hydrocarbons are removed from the deposits before subjecting them to the water and acid steps. If the organics/hydrocarbons are not effectively removed, the subsequent reagents will be unable to contact the deposit. Wet chemistry relies on the ability of the reagents to contact the solid and react, thus removing that component. The weight loss that occurs during this step is used to calculate the weight percent of that specific component. Without adequate contact, these reactions cannot occur; thus, erroneous calculations can result.

Furthermore, it is imperative that all water-soluble salts be removed before exposing the solid to the various acids during the wet-chemistry method. Otherwise, the water-soluble salts will be rinsed off of the deposit following exposure to the acid and reported as a mineral scale instead of a water-soluble salt.

When instrumental methods are used, sample preparation is crucial. Additionally, the instruments need to be maintained in good working order to help prevent erroneous conclusions and affecting the compositional makeup.

Regardless of the procedure used, proper laboratory techniques are necessary for accurate analyses. If inaccurate results are published, incorrect or unnecessary expenses could ensue.

It should also be noted that iron sulfide, upon exposure to atmospheric oxygen, can oxidize to an iron oxide (magnetite). Therefore, it is important that solids samples be transported to the laboratory in a timely manner. Field identification of iron sulfide can be crucial to the laboratory analysis if oxidation has occurred.

#### **Product Residuals**

Product residuals are useful for determining the amount of a chemical that is traveling through a system. However, the presence of a residual does not necessarily imply it is effective. Unless the correct chemical has been selected and applied at the recommended dosage level, the presence of a product can be negligible. Therefore, it is important to understand the product selection process and ensure the correct

product has been identified. Then, through residuals testing, the producer can have confidence in the performance of the production chemical.

The most common product residuals are the corrosion inhibitor and scale inhibitor. These residuals have different interpretations. Corrosion inhibitors are designed to form a film on solid surfaces; therefore, the corrosion inhibitor residual is expected to be lower than the targeted injection rate because some of it would film on the pipe surfaces. This “excess” corrosion inhibitor is therefore captured in the corrosion inhibitor product residual. A positive value on the corrosion inhibitor residual is adequate to ensure the inhibitor has filmed on the metal surfaces. A negative value would indicate there was an inadequate quantity of inhibitor injected and the pipe surfaces might not be adequately protected.

In contrast to the corrosion inhibitor residual, the scale inhibitor value is crucial. Scale inhibitors adhere to the micronuclei scale particles as they begin to form and disrupt the crystal surface or block the growth sites. Phosphate scale inhibitor water sample residuals are acidified, so they are released from the micronuclei scale particles and can then be detected. Inhibitors have a minimum effective dosage (MED), defined by the inhibitor chemistry, product activity, and severity of the scaling issue. When the inhibitor drops below this MED, it can no longer effectively inhibit the deposition of scale. Therefore, the scale inhibitor value reported is important for managing mineral scales.

### Oil and Grease Analyses

A primary use for oil and grease analysis involves compliance with the regulations governing the overboard discharge of produced waters from offshore platforms. However, in addition to this regulatory application, the oil and grease values are of economic importance for onshore facilities, especially water disposal facilities and waterflood systems.

Excessive oil and grease discharged from offshore platforms could result in fines from the Environmental Protection Agency (EPA) (or other regulatory entities) in addition to affecting the company’s public image. Therefore, it is imperative that samples be captured and preserved in accordance with the EPA Method 1664 (2010).

Unless samples are obtained correctly and acidified upon sampling, the results obtained from this method can be erroneous. Non-acidified samples could result in a false low value. Organics and hydrocarbons are often co-precipitated with acid-soluble mineral scales; without acidification, these mineral scales are not dissolved and the oil and grease is not released and therefore unreported. This could have serious regulatory repercussions offshore and result in economic repercussions onshore.

In onshore environments, high oil and grease values can represent revenue losses, such as when oil and grease is carried in a water stream and is injected into a water-disposal well. If oil has been pumped down a well into a nonproducing zone, this could represent a significant loss in oil revenue, depending on the determined quantity of the oil and grease and the volume of water disposed. Additionally, oil and grease can cause plugging in water injection/disposal wells, thereby resulting in costly remediation work.

While the oil and grease values in waterflood injection water do not represent an actual loss in revenue, the injection of oil and grease in the water stream does delay realizing that revenue. Additionally, just as with disposal wells, oil and grease can cause near-wellbore damage that can negatively impact the waterflood and result in costly remediation work to the injection wells.

If water clarification chemicals are used, oil and grease values indicate the effectiveness of this program. Injection rate optimization for water clarifiers is assessed based on oil and grease values, upstream and downstream of the chemical injection. Therefore, correct sampling, preservation, and laboratory techniques are important to help ensure the oil and grease values are accurate and prevent overtreatment of clarification products.



## Corrosion Coupons

Corrosion coupons are one of the most used corrosion monitoring tools in the oil and gas industry. Their preparation, installation, analysis, and interpretation are based on NACE SP0775-2005 (2005). The advantages of using corrosion coupons are numerous.

- They provide visual evidence of the corrosion type in the system at the location tested (pitting, generalized corrosion damage, hydrogen blistering).
- They are a physical measurement of the corrosion rates.
- They can be retained, preserved, or photographed.
- They can be used to measure the response of a system to an operational or treatment modification.

Conversely, there are disadvantages to using corrosion coupons.

- They are a preweighed sand-blasted surface, which is susceptible to contamination that can result in erroneous results (fingerprint, mechanical damage).
- The corrosion rate calculation is a general equation based on weight loss and coupon surface area; it does not consider pitting attack.
- The location within the system is important for the accurate assessment of the corrosion rate.
  - o The coupon represents only that location during the test period in which it was exposed.
- Any weight loss resulting from mechanical damage will be factored into the equation and calculated as corrosion weight loss, artificially increasing the mills-per-year (mpy) corrosion rate.
- Incorrect cleaning of the coupon after removal from the system can result in an erroneous weight-loss calculation.
  - o If solids are not removed and are left on the coupon surface, a low mpy reading can result.
  - o If the cleaning procedure is too aggressive and additional metal is removed during the cleaning process, the mpy rate can be artificially elevated.
- Results are not instantaneous; the coupon should be exposed to the fluids for a minimum of 2 weeks (NACE SP0775-2005 2005); maximum 180 days (49 CFR 192.477 2010).
- The corrosion rate determined on the coupon is a measurement of the corrosion rate on that material at that location.
  - o Interpretation of the coupon mpy is crucial. This mpy rate is not literally applied to the material within the system but is an indicator of the severity of the corrosion that system might be experiencing.

When handled correctly, inserted at the proper location, and analyzed in accordance with NACE SP0775-2005 (2005), coupons are a viable tool for assessing corrosion in a system. When mpy rates are trended over time, coupons are excellent for determining the system's response to a modification—chemical or operational practice change. In chemical treatments, coupons can be used to quantify the response of the system to these changes, whether positive or negative.

### *Recognition of Possible Anomalies in Coupon Analyses*

Tracking and trending the coupon results over time is crucial for identifying possible anomalies. Comparing the mpy rates to the failure rates for a well or field can help validate the mpy reading as a viable measurement for corrosion rates. Furthermore, it can be used to define the well or field key performance indicator (KPI), or tolerance, to corrosion. While NACE SP0775-2005 (2005) defines the corrosion rate interpretation, relating the coupon mpy to failure rates in real time for that coupon location reveals the actual tolerance of the system to the mpy rate. This tolerance for corrosion will, of course, be heavily influenced by economic factors (cost of failures), environmental exposure risks (air/ground/water contamination potentials), or personnel or population exposure (likelihood of injury or fatalities to employees or the public) risk factors; however, a tolerance can be determined.

Without tracking the coupons over time, the overall trend cannot be as easily determined (Ogden, 2006). If trended regularly, an analyst can quickly determine if the mpy result is within historical averages

(statistical process control) for that location. If it is not within the historical average, changes during the current testing cycle need to be considered. Through tracking and trending these mpy readings, anomalies can be quickly identified and corrective action can be made to determine if this anomaly is “real” or a statistical error. Furthermore, conversations between the operator and chemical company are initiated to determine if operational or unscheduled chemical rate changes have occurred during the test period, subsequently explaining the anomaly. Figure 5 shows an example of coupon trending.

## Bacterial Enumeration

Microbiologically influenced corrosion (MIC) is a term used to designate corrosion resulting from the presence and activities of micro-organisms. While micro-organisms do not produce a unique type of corrosion, they can be involved in the degradation of both metallic and non-metallic materials. They produce a localized attack on surfaces that can include pitting, de-alloying, stress cracking, and hydrogen embrittlement. Therefore, monitoring and controlling the bacterial population is crucial for reducing the occurrence of MIC failures.

Monitoring for bacterial growth can be complicated and confusing. Accurate testing is dependent on the sampling technique, procedure, and interpretation of the results. Microscopic, culturing, and immuno-chemistry techniques are all options for the enumeration of bacteria. However, each of these procedures can yield unique and somewhat confusing results from the same sample. Understanding their advantages, disadvantages, and limitations can help select the best process for initial and subsequent bacterial testing.

A microbiologist uses environmental factors to isolate and study micro-organisms. When a nutrient solution of known composition is inoculated with a mixed microbial population, the principle of natural selection begins to operate and the microbe that grows best under the conditions provided soon predominates. As a result of its growth and the chemical changes brought about by its metabolic processes, the medium substrate composition changes and a new predominate microbe will emerge that grows best under these conditions. By carefully selecting and maintaining a set of conditions and providing a specific nutritional media, any naturally occurring micro-organism can be isolated. This principle is the basis by which all micro-organisms are studied and isolated.

Because bacteria vary greatly in their nutritional needs, no single medium is capable of supporting growth of more than a small fraction of the bacteria that exist in nature. Therefore, if bacteria are suspected, yet no growth is noted within standard culture vials, a specialized broth or enumeration technique might be required to verify their existence.

The enumeration tests conducted are based on NACE TM0194-2014 (2014), which is the industry-standard serial dilution test method. Even if other enumeration techniques are used, it is recommended that the technician inoculate the serial dilution broth bottles for a comparison in compliance with NACE TM0194-2014 (2014).

This enumeration technique uses a common culture media to determine the broadest classification of bacteria (i.e., sulfate-reducing, acid-producing, or general aerobic bacteria), not the specific bacterial species.

NACE TM0194-2014 (2014) contains the specific formulation for preparing the serial dilution broth bottles. It should be noted that some strains of bacteria might necessitate specific specialized broths. If this is the case, a broth can be made to better replicate the produced water and its associated nutrients (i.e., some strains of sulfate-reducing bacteria (SRB) require the addition of organic acids as a nutrient to facilitate growth). Viable bacteria are necessary for this technique, and it is the only method available to measure viable bacteria only, which highlights several limitations to this technique.

- Culturing time is necessary for these cells to replicate within the vials. Therefore, 2 to 4 weeks of incubation is necessary to reach completion.
- The correct saline broth should be used (matched closely to the salinity of the produced water).

- Incubation temperatures might need to be modified to better represent the system.
- When flowing water is tested, the bacteria captured and inoculated will be the planktonic (floating) bacteria in the water stream and not the sessile (attached) bacteria adhering to the pipe/vessel wall surfaces.

Other techniques can be used to determine total bacteria counts, such as the adenosine triphosphate (ATP) method. This technique is based on the metabolism of the living bacterium, which uses this high-energy molecule in large quantities. This method calls for extracting the ATP from the cell, reacting it with a standard quantity of luciferin-luciferase, and measuring the light units produced with a photometric analyzer. These light units can then be compared throughout a field or lease to identify areas of high metabolic activity; however, this technique cannot differentiate between the various strains of bacteria.

Other methods, such as RapidChek® SRB immunoassay test kits, Sani-Check® SRB/APB test kits, fluorescence microscopy, fluorescence in-situ hybridization, and advanced genetic techniques for the identification of bacterial species, can be used to identify bacteria. Each technique produces results unique to that specific procedure; therefore, the results from one test method should not be intermixed with the results from another test method.

In review of the typical methods of identifying the types of bacteria, microscopic examination and staining techniques obviously do not lend themselves readily to field evaluations. Additionally, most culturing techniques are not easily performed in the field, with the exception of the NACE serial dilution technique.

#### *Recognition of Possible Anomalies in Bacterial Analyses*

A common error in the enumeration of bacteria is contamination during the sample gathering and/or testing procedure. Analysts must use sterile syringes when performing the serial dilution technique to help ensure no contamination is introduced into the culture vials. Additionally, if using the ATP or immunoassay techniques for enumeration, it is imperative that the analyst use consistent techniques to prevent inconsistent results.

Furthermore, all culture vials and reagents used in these tests have a shelf-life, or expiration date. This shelf-life is a function of not only the age of the vials/reagents but also the conditions of the environment in which they are stored. Therefore, it is crucial that the analyst ensure all equipment, culture vials, and reagents are stored in compliance with the manufacturer's recommendations and are discarded after the expiration date noted on each shipment. Otherwise, erroneous results might be reported, which could result in overconfidence (that no potential problems exist) and treatments being ceased or reduced. This could ultimately result in an increase in bacterial-related failures.

It is also important for the analyst and producer to understand that the fluids used in these enumeration techniques are most commonly extracted from the flowing stream of water; therefore, the results represent the planktonic bacteria. In summary, these methods only enumerate a small fraction of the total bacteria in the water stream compared to what the system might actually contain. Most of the bacteria are sessile (i.e., growing on pipe walls, under scale, in sludges, and at interfaces) and not planktonic (i.e., free floating in the water). Therefore, if the enumeration of sessile bacteria is the goal of the monitoring program, additional equipment (Robbins devices) or modified procedures [NACE TM0194-2014 (2014) contains examples of these sessile techniques] might be necessary.

Ultimately, measuring, tracking, and trending the bacterial counts is crucial to understanding what is occurring in a field, lease, or well, in addition to determining the efficiency of biological control methods (operational and/or chemical). Correlating these numbers to the actual observed bacterial damage or bacterially related well/equipment failures should yield the optimum level of tolerance for that field, lease, or well as it relates to the number of colonies enumerated by the various techniques.

#### CONCLUSIONS

Technology advances enabled an operator and chemical company to analyze fluid constituents and solids to determine their components and probable origins to identify effective management programs for these production challenges. However, it is important that industry standards be used for proper

sampling, handling, and preservation of field fluid samples. Additionally, analysis and interpretation of these analytical tests needs to be performed and communicated accurately.

Tracking and trending analytical results over time makes it possible for anomalies to be quickly and readily discovered. Therefore, retesting can be performed to determine if these anomalies are truly a system or chemical performance change or an error in the sampling/analysis techniques. Identifying the correct response to an anomaly can be the difference between the success or failure of a well or field management program and can impact the future environmental, regulatory, and economic viability of a well or field.

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ACKNOWLEDGMENT

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Table 1 - Common Production Challenges and Associated Analytical Testing

Location	Common Production Challenges	Common Analytical Tests
Downhole	Corrosion Mineral scales/solids Paraffin/asphaltenes Hydrates Bacteria H <sub>2</sub> S/FeS Liquid loading	Water analysis* Metals Product residual Oil analysis/gas analysis Bacterial enumeration test Corrosion coupon (downhole or wellhead) Solids analysis
Surface lines (flowlines, gathering lines, pipelines)	Corrosion Mineral scales/solids Paraffin/asphaltenes Hydrates Bacteria H <sub>2</sub> S/FeS Oxygen	Water analysis* Metals Product residual Oil analysis/gas analysis Bacterial enumeration test Corrosion coupon Solids analysis Oxygen analysis (on gas or water phase)
Production/separation vessels (Free water knock-out; 2- or 3-phase separators, heater-treaters)	Corrosion Mineral Scales/Solids Build-up Paraffin Bacteria H <sub>2</sub> S/FeS Oxygen Water Quality Issues Emulsions	Water analysis* Metals Product residual Oil analysis/gas analysis Bacterial enumeration test Solids analysis Oxygen analysis (on gas or water phase) Oil and grease (gravimetric method)
Oil stock tank	Corrosion (water phase/bottom of tank/vapor phase) Paraffin/Asphaltenes Bacteria (in water phase) H <sub>2</sub> S/FeS Oxygen (vapor phase) Emulsions Bottoms (Solids) Build-up	Oil analysis Solids analysis Oxygen analysis (on gas or water phase) Oil quality determination (API grindout)
Water storage tank	Corrosion Mineral scales/solids Bacteria H <sub>2</sub> S/FeS Oxygen Water quality issues Bottoms (solids) buildup Oil carry-over/skimming issues	Water analysis* Metals Product residual Oil analysis/gas analysis Bacterial enumeration test Solids analysis Oxygen analysis (on gas or water phase) Oil and grease (gravimetric method) Suspended solids (membrane test)
Water injection well or salt water disposal well/injection or disposal pumps	Corrosion Mineral scales/solids Bacteria H <sub>2</sub> S/FeS Oxygen Water quality issues Oil carry-over TSS	Water analysis* Metals Product residual Oil analysis/gas analysis Bacterial enumeration test Solids analysis Oxygen analysis Oil and grease (gravimetric method) Suspended solids (membrane test)

\*All unstable components should be analyzed immediately upon sampling in accordance with API RP-45 (1998).

Table 2 - Primary Constituents of Oilfield Waters

Cations	Anions	Other Properties
*Calcium (Ca) *Magnesium (Mg) *Sodium (Na) *Iron (Fe) *Barium (Ba) Strontium (Sr) Manganese (Mn)	*Chloride (Cl) *Carbonate (CO <sub>3</sub> ) *Bicarbonate (HCO <sub>3</sub> ) *Sulfate (SO <sub>4</sub> )	*pH *Temperature *Specific gravity *Dissolved carbon dioxide *Sulfide as H <sub>2</sub> S Resistivity Dissolved oxygen Bacterial population Oil content Turbidity Suspended solids—amount, size, shape, chemical composition

(\*) Essential components for obtaining a thorough and meaningful water analysis

Table 3 - Relative Solubilities of Mineral Scales in Distilled Water, Atmospheric Pressure

Mineral Scale	Solubility (mg/L) in Water
Calcium sulfate (gypsum) (CaSO <sub>4</sub> · 2H <sub>2</sub> O)	2080
Calcium carbonate (CaCO <sub>3</sub> )	53
Barium sulfate (BaSO <sub>4</sub> )	2.3

Table 4 - Primary Variables in the Formation of Mineral Scales

Scale or Deposit	Chemical Formula	Primary Variables
Calcium carbonate	CaCO <sub>3</sub>	<ul style="list-style-type: none"> <li>Partial pressure of CO<sub>2</sub> (scale increases as CO<sub>2</sub> decreases)</li> <li>Less soluble with increasing temperatures</li> <li>Pressure reductions</li> <li>More soluble as TDS increases</li> </ul>
Calcium sulfate	CaSO <sub>4</sub> · 2H <sub>2</sub> O (gypsum) CaSO <sub>4</sub> (anhydrite)	<ul style="list-style-type: none"> <li>Less soluble at temperatures higher than 50°C</li> <li>Pressure reductions</li> <li>More soluble as TDS increases</li> </ul>
Barium sulfate	BaSO <sub>4</sub>	<ul style="list-style-type: none"> <li>More soluble as temperatures increase</li> <li>More soluble as TDS increases</li> </ul>
Strontium sulfate	SrSO <sub>4</sub>	<ul style="list-style-type: none"> <li>Solubility decreases as temperatures increase</li> </ul>
Iron Compounds: Iron carbonate Iron sulfide Iron (II) hydroxide Iron (III) hydroxide Iron oxide	FeCO <sub>3</sub> FeS Fe(OH) <sub>2</sub> Fe(OH) <sub>3</sub> Fe <sub>2</sub> O <sub>3</sub>	<ul style="list-style-type: none"> <li>Corrosion by-products</li> <li>Bacterial activity</li> <li>Dissolved gases</li> <li>Depositions increase as pH increases</li> </ul>

Table 5 - Common Suspended Solids and Their Probable Origins

	Hydrocarbons	Iron Compounds	Carbonates	Sulfates	Insolubles
Analysis detail	<ul style="list-style-type: none"> <li>Oil carry-over</li> <li>Paraffin</li> </ul>	<ul style="list-style-type: none"> <li>Iron sulfide</li> <li>Iron oxide</li> <li>Iron carbonate</li> </ul>	<ul style="list-style-type: none"> <li>Calcium carbonate</li> <li>Iron carbonate</li> <li>Magnesium carbonate</li> </ul>	<ul style="list-style-type: none"> <li>Calcium sulfate</li> <li>Magnesium sulfate</li> </ul>	<ul style="list-style-type: none"> <li>Barium sulfate</li> <li>Formation fines</li> <li>Sand</li> <li>Microbes</li> <li>Asphaltenes</li> <li>Completion fluid returns</li> </ul>
Possible origin(s)	<ul style="list-style-type: none"> <li>Separator malfunction</li> <li>Truck treating schedules</li> <li>Surface tank or vessel damage</li> <li>Improper equipment sizing</li> </ul>	<ul style="list-style-type: none"> <li>Corrosion</li> <li>Mixture of incompatible waters</li> <li>Oxygen introduction</li> <li>Stimulation by-products</li> </ul>	<ul style="list-style-type: none"> <li>Scaling waters</li> <li>Corrosion</li> <li>Pressure reductions with subsequent scale deposition</li> <li>Fluid property changes</li> </ul>	<ul style="list-style-type: none"> <li>Scaling water</li> <li>High temperatures</li> <li>Pump outlets/shrouds</li> <li>Ineffective cooling of downhole electric submersible pumps (ESPs)</li> <li>Incompatible waters</li> </ul>	<ul style="list-style-type: none"> <li>Scaling</li> <li>Mixing incompatible waters</li> <li>Pump intakes set low</li> <li>Bacterial activity</li> <li>Dead bacteria (following a biocide application)</li> <li>Biofilm</li> <li>Natural, or induced, formation of asphaltenes (CO<sub>2</sub> flood)</li> </ul>

Table 6 - Solubilities of Oilfield Deposits

Scale Type	Chemical Formula	Mineral Name
<b><i>Water-Soluble Deposits</i></b>		
Sodium chloride	NaCl	Halite (salt)
<b><i>Hydrochloric Acid-Soluble Deposits</i></b>		
Calcium carbonate	CaCO <sub>3</sub>	Calcite
Iron carbonate	FeCO <sub>3</sub>	Siderite
Iron sulfide	FeS	Trolite
Iron oxides	Fe <sub>3</sub> O <sub>4</sub>	Magnetite
	Fe <sub>2</sub> O <sub>3</sub>	Hematite
<b><i>Hydrochloric Acid-Insoluble Deposits</i></b>		
Calcium sulfate	CaSO <sub>4</sub> * 2 H <sub>2</sub> O	Gypsum
Calcium sulfate	CaSO <sub>4</sub>	Anhydrite
Barium sulfate	BaSO <sub>4</sub>	Barite
Strontium sulfate	SrSO <sub>4</sub>	Celestite
Barium strontium sulfate	BaSr(SO <sub>4</sub> ) <sub>2</sub>	Barium strontium sulfate



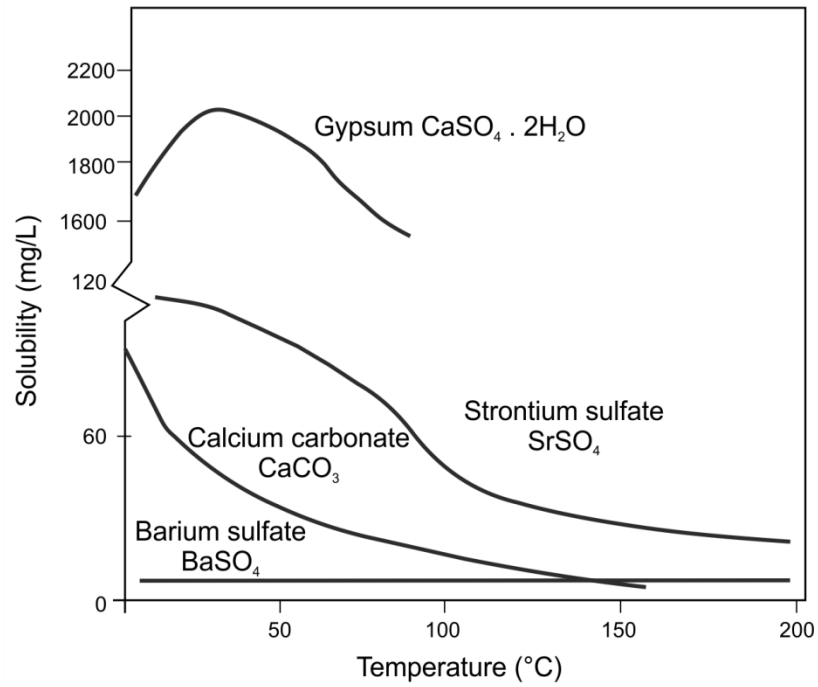


Figure 1 - Scale Solubilities in Water as a Function of Temperature

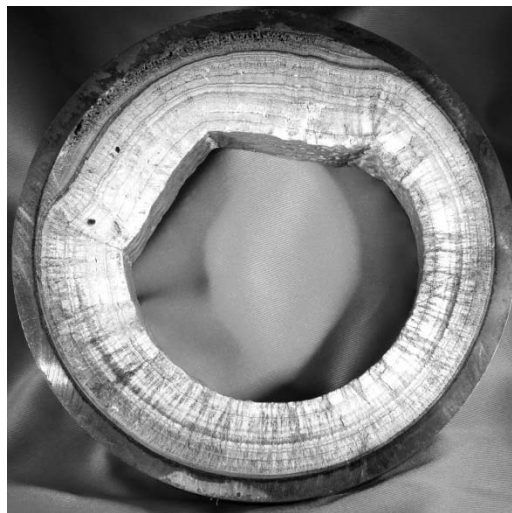


Figure 2 - Calcium Carbonate Scale



Figure 3 - Calcium Sulfate (Gypsum) Scale



Figure 4 - Barium Sulfate Scale

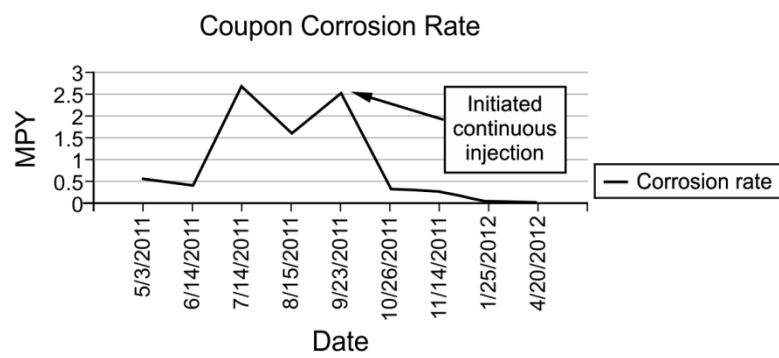


Figure 5 - Illustration of Coupon Trending Over Time