THE EFFECT RELIEVING CASING PRESSURE HAS ON BOTTOMHOLE PRESSURE

Charlie D. McCoy, Mark Lancaster and Joey Boyd Permian Production Equipment, Inc.

ABSTRACT

We will show in multiple case studies the effect of relieving back pressure on an oil well has in relationship to the producing bottomhole pressure, pump efficiency and over all economics of the well. This will be done by utilizing a Beam Gas Compressor®, BGC.

HISTORICAL DEVELOPMENT

Doing a fluid shot with an echometer device has long been the standard for determing the amount of fluid above the pump, pump efficiency, downhole pressures and many other items. In this paper we will discuss the changes that occur when the casing pressure is minimized by utilizing a Beam Gas Compressor® or BGC. The BGC uses a single cylinder to reduce the pressure in the annulus of the sucker rod pumped well and then discharges the gas back into the surface flowline or sales line. The resulting removal of the backpressure on the formation allows more gas to flow at a quicker rate, while also improving the efficiency of the downhole pump with greater fillage percentages. The pumping unit uses the torque creation of its prime mover at the middle of each stroke and the BGC takes advantage of this torque at the top and bottom of the stroke.

BASIC DESCRIPTION

To properly design a rod string you must understand how the well will react when pressure is added, via a choke, or reduced via venting or use of a BGC. Many people operate with the theory adding back pressure can reduce gas interference where by the exact opposite is true under the right conditions. You can often see how a well was originally designed does not work out to optimization. That is the point of continuing to do fluid shots at a consistent time period to see how the well changes as it produces. Producing rates can be estimated within the desired range of accuracy using the IPR technique with two stabilized producing rates and corresponding stabilized producing pressures. This makes it possible to use the IPR without needing to shut in the well and lose production to obtain shut-in information. Obtaining a bottomhole pressure equal to 10% of the shut-in reservoir pressure is recommended for determining maximum production rates for sucker-rod lifted wells. At this pressure, the maximum well productivity will be 97% of the well's theoretical maximum production rate.

LET'S FIRST LOOK AT THE PARTS OF A FLUID SHOT REPORT

The report consists of two pages Liquid Level (fig. 1) and the Dyno Page (fig. 2)

The Liquid Level pages shows how many feet above the pump the liquid is and how much free gas is in that liquid. It also shows the amount of casing pressure and annular gas flow. This is important as you can easily determine if a well is slugging gas up the tubing by comparing this information to the amount of gas the well is selling. Also you can gather the producing bottom hole pressure (PBHP) and the static bottom hole pressure (SBHP). Often the SBHP is not attainable unless the well has been shut down for a period of time.

You can also see the pressure rate of gas buildup, this is important when sizing the right size of wellhead compressor.

The Dyno Page shows the effectiveness of the downhole pump, rod loading and gas displacement. You will see how much pressure is being placed on the Tubing by possibly using a choke and the pressure on the Casing. The

Casing pressure is generally the same as flowline. Beam Loading is also indicated on this page, as well as, FoMax (which is the optimum level of fluid production).

NOW LET'S LOOK AT THE HOW DESIGN SOFTWARE SHOWS IT SHOULD OPERATE

In Figure 3 you can see how the original design of the rod string would generate the capabilities of the well. This information is gathered by looking at the current rod string and the pumping unit. This would be the maximum capacity of this unit. Let us compare that with the fluid shots taken before the BGC was installed. It is easy to see that the structure of the well could produce much more oil and gas if the formation was able to move the fluid to the well bore. The pressures in the formation may no longer be sufficient.

LET'S LOOK AT THE BEFORE FLUID SHOTS

Most notably you will see the amount of gas calculated to flow up the annulus. What percentage is this of the total reported by the operator? The difference is the amount of gas flowing up the tubing and creating the inefficiencies in the pump. With the installation of the BGC this will change as the majority of gas is drawn up the annulus.

In some versions you can see the amount of gas and fluid as it moves in the pump, Figure 4 a and b. The top photo shows a pump with gas interference and the bottom shows fluid now in the pump after installation of a Beam Gas Compressor. You can see the increase plunger travel which results in greater oil production as well as a fuller pump.

PBHP this number is very important to determine the amount of fluid increase you can achieve by lowering the casing pressure. A current IPR (Inflow Performance Relationship) is often difficult to obtain but a ratio can be derived by looking at the PBHP and the Pump Intake Pressure (PIP). Most people believe that the PBHP should be less than 10% of the static bottomhole pressure (SBHP) 1. This is to achieve maximum production. As wells are depleted the SBHP becomes a closer relationship to the PBHP and it must be artificially changed by using a form of wellhead compression if the well is to continue to be profitable. By artificially lowering the PBHP you can greatly increase the flow of fluid to the well bore.

Casing pressure buildup is an interesting aspect as it will allow you how to set the timers or the pump off controller to maximize the effect of the lowered casing pressure. If for example a well operates 50 minutes on and 50 minutes off... the question would be how quickly does the well build back up to the original pressure... it may be necessary to adjust the run times to 25 minutes on and 25 minutes off to maximize the lowest continual casing pressure (LCCP)

By determing the LCCP it will allow for the well to have the greatest possible time in a 24 hour period with the lowest possible PBHP.

CASE STUDIES

Number 1- The casing pressure was over 200 psig when a beam gas compressor was installed the casing pressure reduced over 132 points. The gas increase flowing up the annulus was 366 mcfd. This well was sending a larger amount of gas up the tubing now the BGC is drawing it all up the annulus and providing more opportunity for pump fillage.

Pump Intake and Producing Bottom Hole Pressure decreased in excess of 180 psig. This allowed for an increase in oil flow from the formation to the well bore and then up the pump as it no longer was clogged with gas.

The amount of pressure at the gas/liquid interface decreased by over 125 psig with a resulting lowering of the liquid level by 600 feet. This lowering of the liquid level is also part of the lowering of the producing bottom hole pressure.

Number 2- In this case it is easy to see the increase of the velocity of gas now being produced in the well bore. This increased velocity will aid in the use of gravitational separators. You can also see the full amount of gas is now traveling up the well bore and no longer up the tubing.

Number 3- In this case you also have a lowering of casing pressure and a subsequent increase of fluid production which is attested to by increase run time. You also see an increasing of bottom hole pressures which is attributed to the increase fluid level and more fluid coming to the well bore.

You can also see the loading of the pumping unit is lessened by the use of the BGC. In the pumping action of the sucker rod pumping unit on its upstroke the BGC is also compressing gas into the same fluid flow line. Thereby reducing the restriction the fluid has to move thru the line.

With the lowering of the loading you see a subsequent reduction of horse power usage. Interesting enough here you get an increase of PBHP as more fluid is now in the wellbore.

Number 4- As in the previous examples a reduction of casing pressure resulted in an increase oil and gas production and reduction in loading and horsepower usage.

Number 5- This well also shows an increase of the velocity of gas, lower casing pressure, greater production and a reduced PBHP. This is interesting when looking at the effect gravitational gas separators have on the production of a rod pumped well... Most of them depend on the velocity of the gas to escape their fluid captors to rise to the surface. If the velocity is not great enough it will stay in the fluid and go up the pump. In all of the case studies you see a tremendous increase in the velocity of the gas as shown by the echometer system.

Number 6- This case also shows the increase of the velocity of gas. This will allow a customer who has previously invested into a separator to now increase the effectiveness of that piece of equipment by installing a BGC. It also shows that reducing the backpressure would increase the drawdown and the well productivityⁱⁱ.

IN CONCLUSION

Reduction of casing pressure has long been proven as a means for increasing oil production. The main way of doing that was by opening the vent pipe and releasing the back pressure to atmosphere. With the Beam Gas Compressor you are able to accomplish the same purpose but environmentally safely capture the gas and get rid of the pressure. By utilizing testing equipment you can easily see the effect of lowering casing pressure on a well bore. The interesting applications are the lowering of the loading and horsepower for the pumping unit which should translate to a longer life and less breakdown of the pumping unit and rod string.

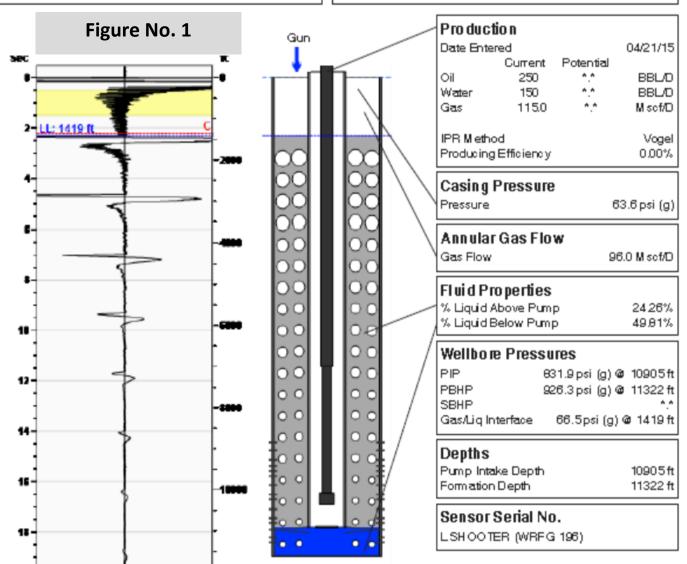
Another method of effecting a change on the bottomhole pressure was to put significant back pressure on the tubing. This cause premature packing failure and often rod collapse and pump failures. This also can be minimized by using a BGC to reduce casing pressure and thereby increase the differential between well bore and formation.

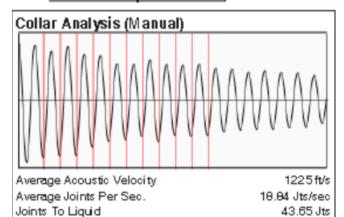
In addition the showcase of increasing the velocity of the gas up the annulus can only be seen as a tremendous way to minimize the amount of gas going up the tubing. Many companies have installed "Mother Hubbard" or Gas Separators. These devices are very effective until the gas velocity reduces with a BGC you can artificially increase this velocity and enjoy greater separation of fluid and gas for a longer duration.

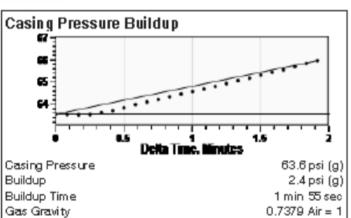
Liquid Level

1419 ft

Fluid Above Pump	9406 ft
Equivalent Gas Free Above Pump	2301 ft

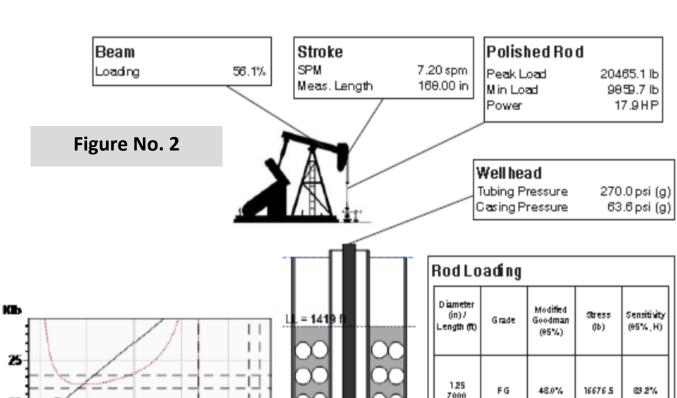






Comments and Recommendations

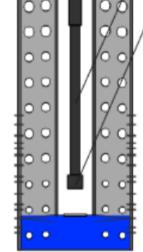
100% run time



25
20
10
5
0 50 100 150 200

Production Oil 250 BBL/D Water 150 BBL/D Gas 115 BBL/D

System Efficiencie	es
Polished Rod/Miotor Eff.	. ^.*
Pump/Motor Eff.	^.^
Volumetric Eff.	94.9%



Pump (API: 0-150 R?B? 30-4)

49.1%

14.5%

10069.2

2019.5

44.4%

6.6%

D

58

8075

15

Max Stroke Length 233.72 in Effective Plunger Stroke 221.91 in Effective Fillage 94.9% Effective Displacement 419 BBL/D

 Calculated Fluid Load Max
 9245.3 lb

 Pump Fluid Load, Fo(Up-Dn)
 1393 lb

 Damp Up 0.15905
 Damp Dn 0.15905

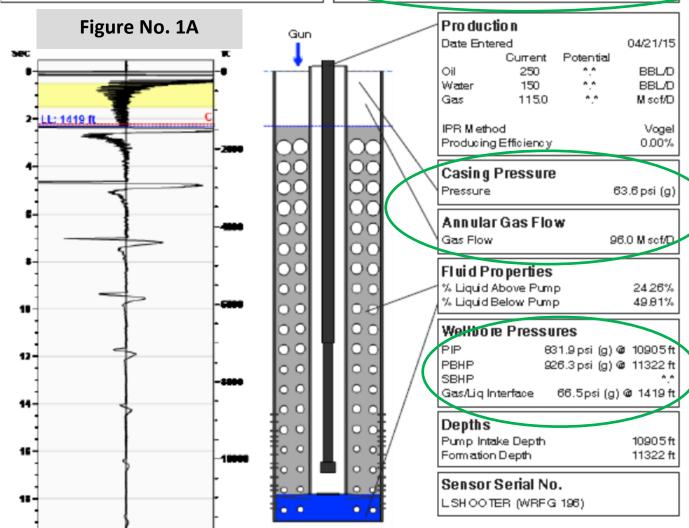
 Kr
 90 lb/in

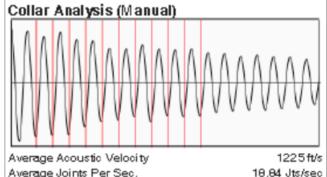
 Kt
 595955 lb/in

Pump Intake Pressure 4443.4 psi (g)
Pump HP 8.5 HP

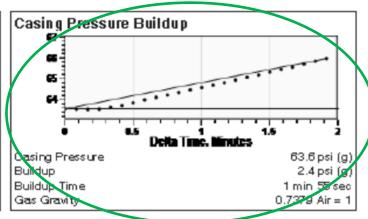
Comments and Recommendations





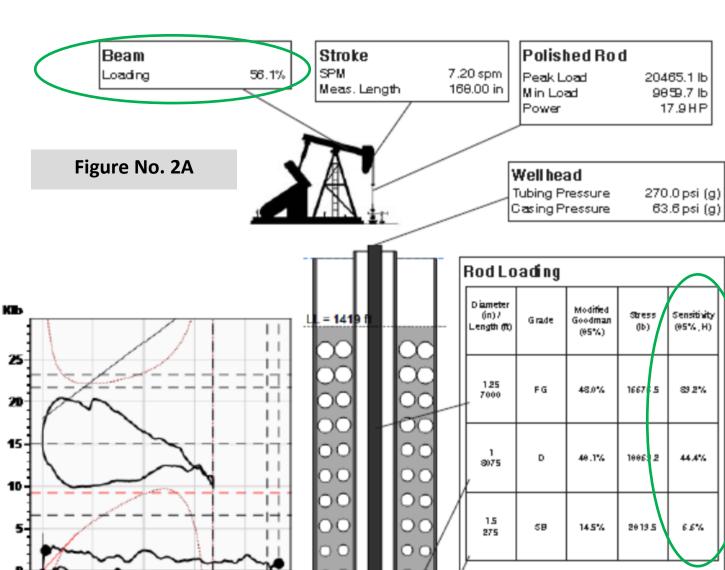






Comments and Recommendations

100% run time



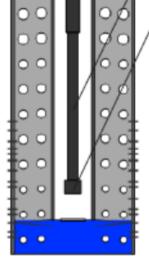
P roduction

Oil 250 BBL/D Water 150 BBL/D Gas 115 BBL/D

200

System Efficiencies

Polished Rod/Motor Eff. ^.*
Pump/Motor Eff. ^.*
Volumetric Eff. 94.9%



Pump (API: 0-150 R?B? 30-4)

Max Stroke Length 233.72 in Effective Plunger Stroke 221.91 in Effective Fillage 94.9% Effective Displacement 419 BBL/D

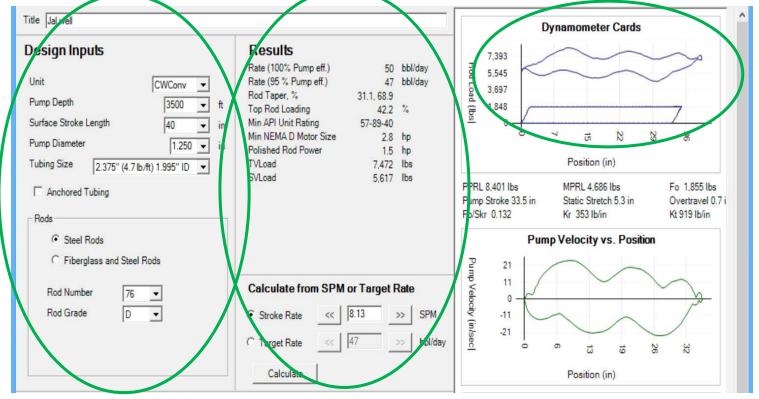
Calculated Fluid Load Max 9245.3 lb Pump Fluid Load, Fo(Up-Dn) 1393 lb Damp Up 0.15905 Damp Dn 0.15905 Kr 90 lb/in Kt 595955 lb/in

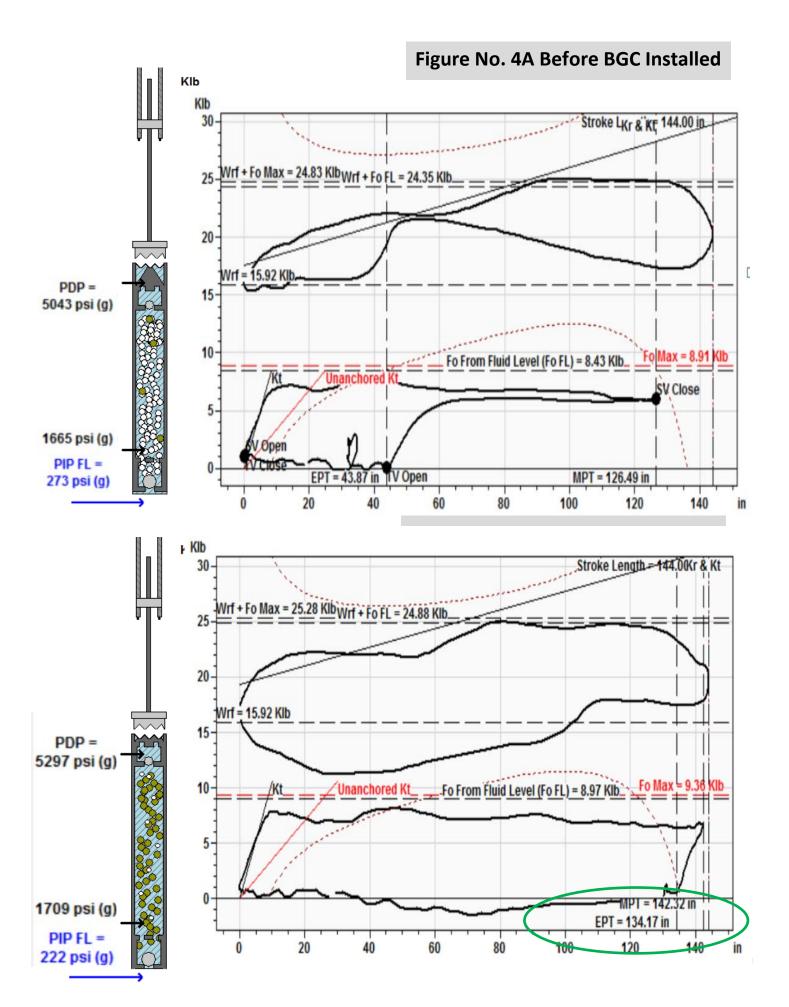
Pump Intake Pressure 4443.4 psi (g) Pump HP 8.5 HP

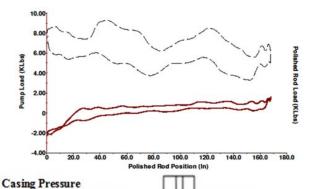
Comments and Recommendations

Figure No. 3









Case Study Number 1

202.7 psi (g)
Casing Pressure Buildup
23.4 psi (g)
1.00 min
Gas/Liquid Interface Pressure
217.2 psi (g)
Liquid Level Depth
2740.31 ft
Pump Intake Depth
3574.00 ft
Formation Dep th
3536.00 ft

Formation Submergence
Total Gazeou: Liquid Column HT (TVD) \$34 ft
Equivalent Gaz Free Liquid HT (TVD) 187 ft
Acountic Test

Producing Annular Gas Flow 67.5 MscFD % Liquid

Pump Intake

285.1 psi (g)

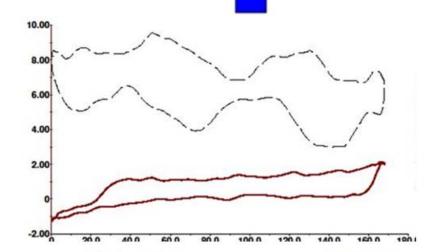
19 %

Producing BHP

2713 psi (g)

Static BHP

480.0 psi (g)



Casing Pressure 70.5 psi (g) Casing Pressure Buildap 15.0 psi (g) 1.00 min

Gas/Liquid Interface Pressure 78.0 psi (g)

Liquid Level Depth 3384.07 ft

Pump Intake Depth

3574.00 ft

Formation Depth 3536.00 ft

Formation Submergence
Total Gazeou: Liquid Column HT (TVD) 190 ft
Equivalent Gaz Free Liquid HT (TVD) 67 ft
Acoustic Test

Producing Annular Gas Flow 434 MscFD

% Liquid

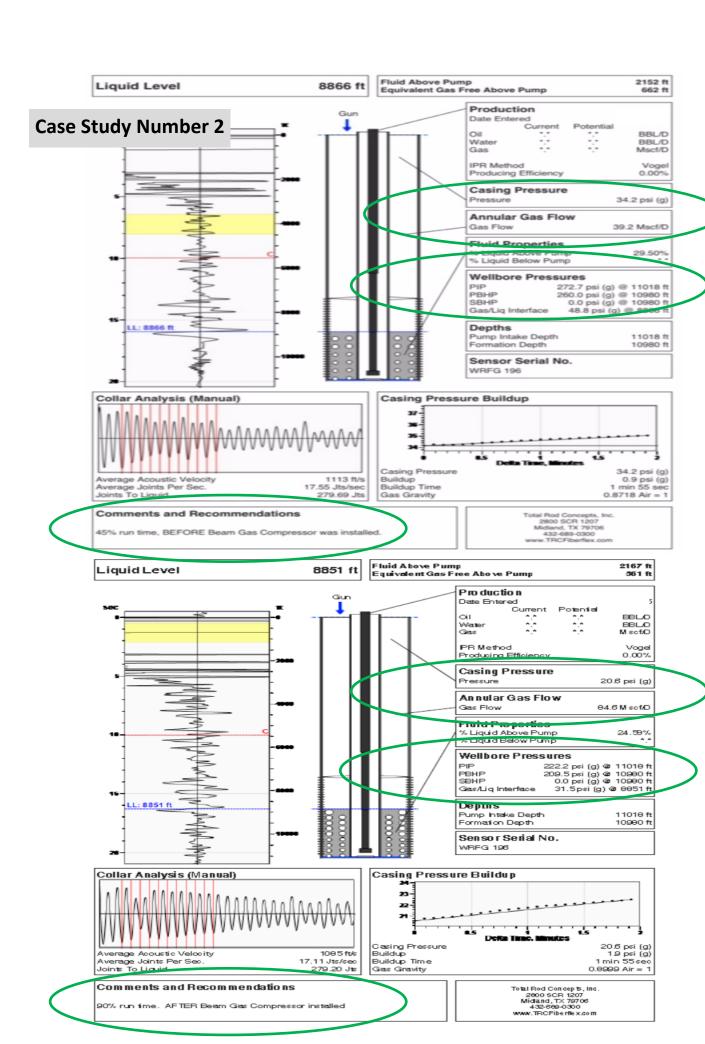
Pump Irrake

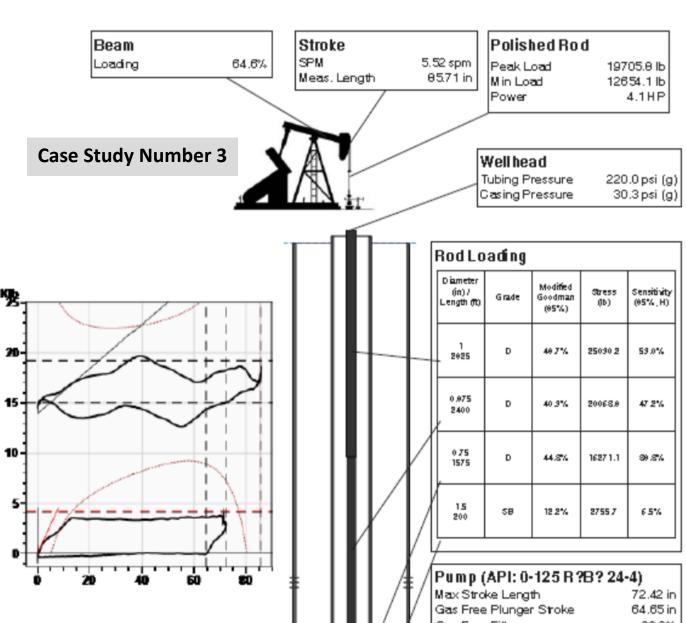
102.5 psi (g)

Producing BHP

88.6 psi (g) Static BHP

397.3 psi (g)





Production

 Oil
 ^.* BBL/D

 Water
 ^.* BBL/D

 Gas
 ^.* BBL/D

System Efficiencies

Polished Rod/Motor Eff. ^.^
PumpMotor Eff. ^.^
Volumetric Eff. 89.3%

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Gas Free Plunger Stroke 64.65 in
Gas Free Fillage 99.3%
Gas Free Slippage 11 BBL/D
Gas Free Displacement 52 BBL/D

 Calculated Fluid Load Max
 4217.6 lb

 Pump Fluid Load, Fo(Up-Dn)
 3478 lb

 Damp Factor
 0.12070

 Kr
 226 lb/in

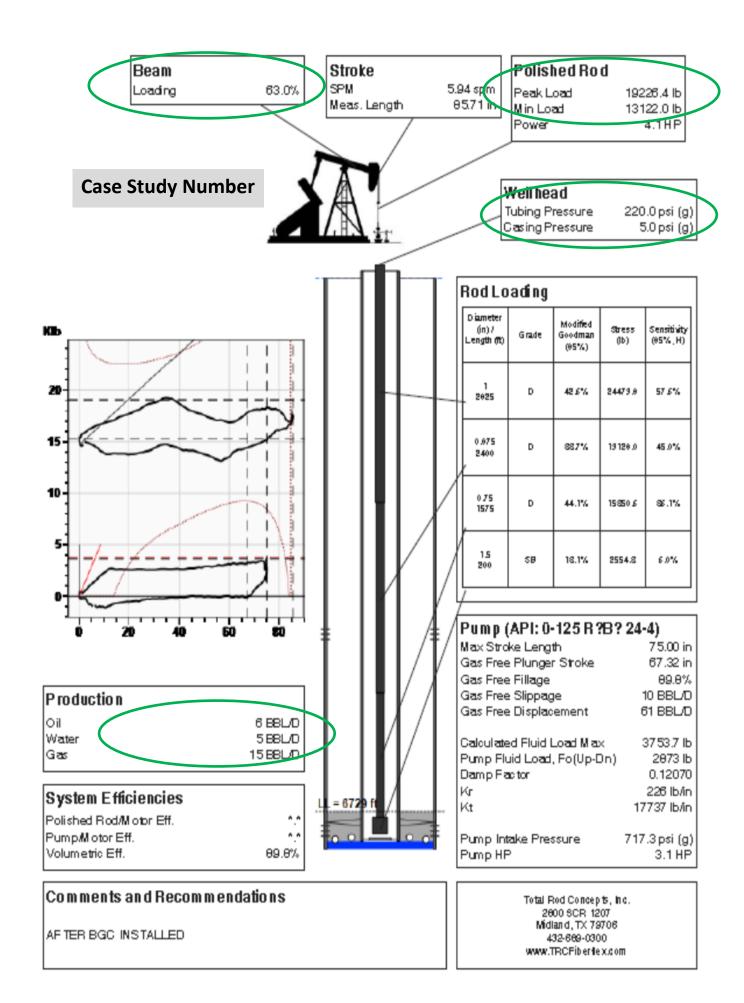
 Kt
 17737 lb/in

Pump Intake Pressure 603.0 psi (g) Pump HP 3.2 HP

Comments and Recommendations

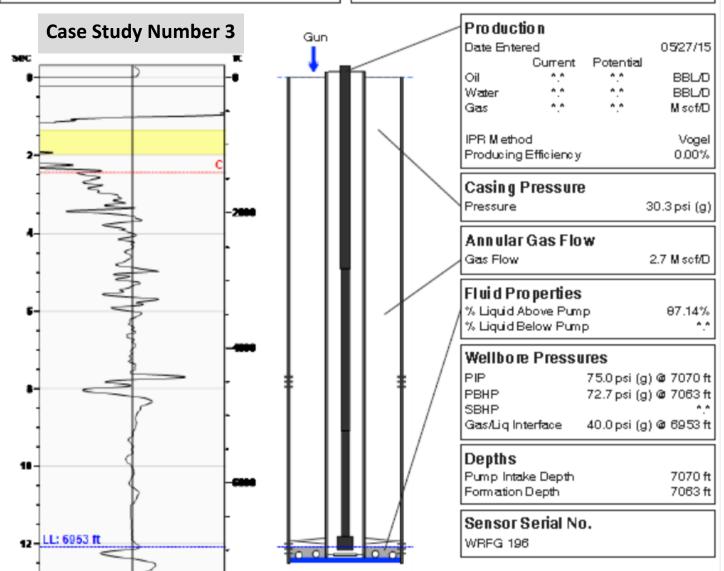
BEFORE BGC WAS INSTALLED

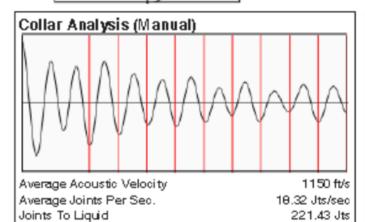
2 BBL/D 2 BBL/D 12 BBL/D

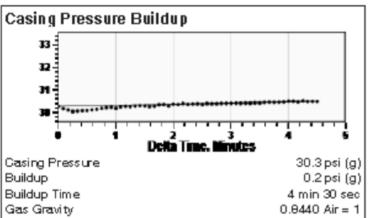


Liquid Level 6953 ft

Fluid Above Pump 117 ft Equivalent Gas Free Above Pump 103 ft







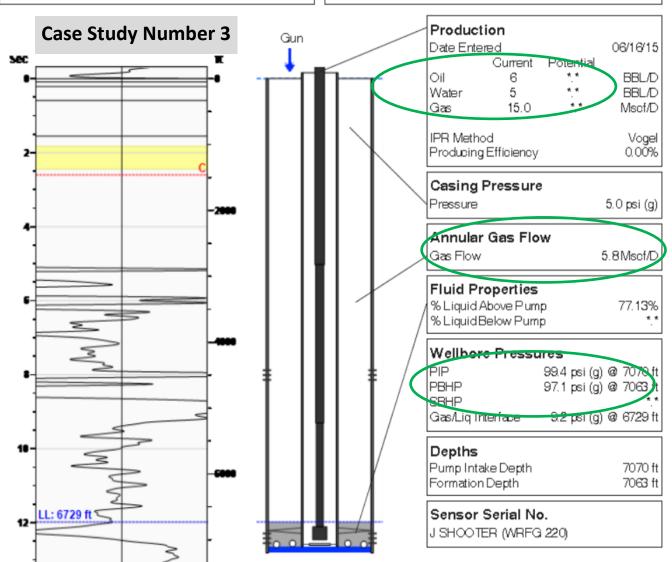
Comments and Recommendations

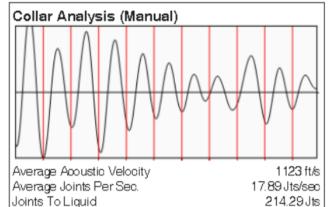
60% RUNITIME, BEFORE BGC WAS INSTALLED

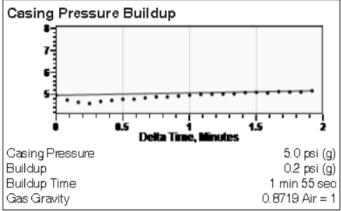
2 BBL/D 2 BBL/D 12 BBL/D

Liquid Level 6729 ft

Fluid Above Pump 341 ft Equivalent Gas Free Above Pump 265 ft

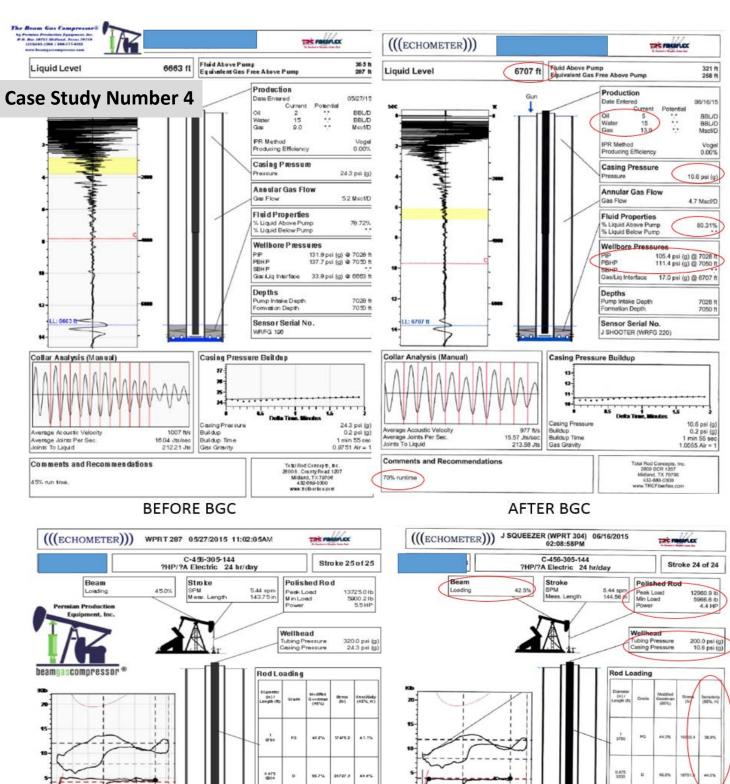


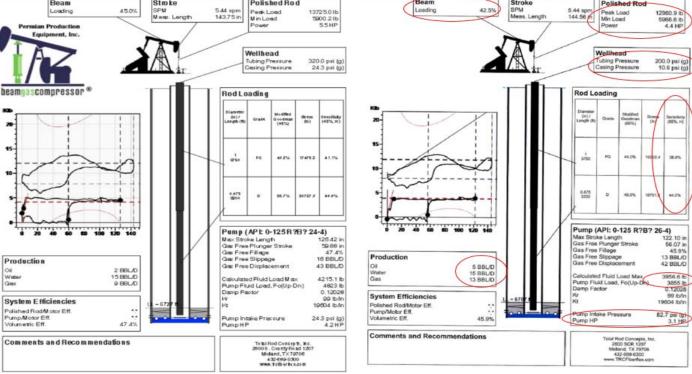




Comments and Recommendations

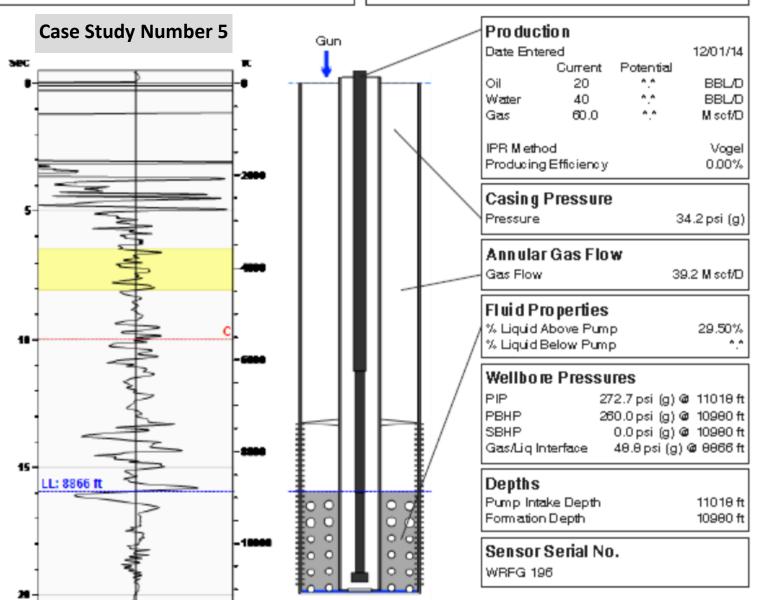
SET ON HAND. AFTER BGC WAS INSTALLED

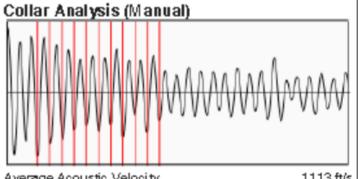




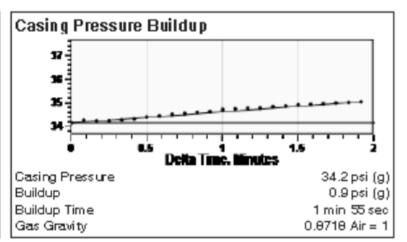
Liquid Level 8866 ft

Fluid Above Pump 2152 ft Equivalent Gas Free Above Pump 662 ft





Average Acoustic Velocity 1113 ft/s
Average Joints Per Sec. 17.55 Jts/sec
Joints To Liquid 279.69 Jts

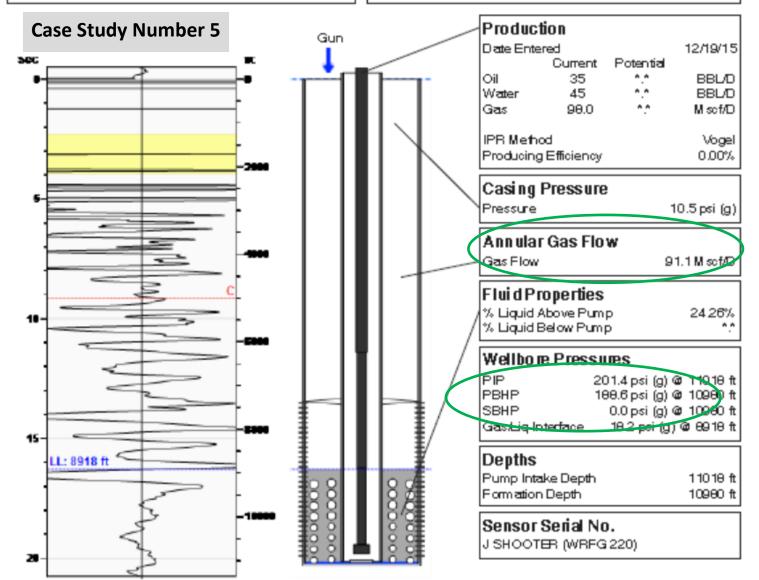


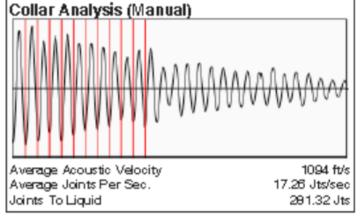
Comments and Recommendations

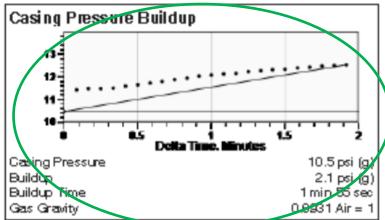
45% RUNITIME, BEFORE BGC WAS INSTALLED

Liquid Level 8918 ft

Fluid Above Pump 2100 ft Equivalent Gas Free Above Pump 530 ft







Comments and Recommendations

90% run time. AFTER BGC installed



Stroke SPM 7.38 spm Meas, Length 144.00 in

Polished Rod

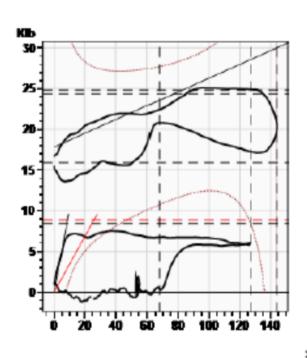
Peak Load 25112.9 lb Min Load 13615.0 lb Power 14.2HP

Case Study Number 6



Wellhead

Tubing Pressure 28.4 psi (g) Casing Pressure 34.2 psi (g)



Rod Loading

	Diameter (in)/ Length (ft)	Grade	Modified Goodman (95%)	Stress (lb)	Sensitivity (95%, H)
-	125 6287	FG	51.6%	20468.9	49.2%
	1 2650	D	60 7%	259943	612%
	0.975 1750	D	72.7%	210205	51.8%
1	1£25 200	5B	22.5%	4416.4	10 4%

Production

Oil Water *.* BBL/D Gas

^.^ BBL/D *.* BBL/D

System Efficiencies Polished Rod/Miotor Eff. Pump.M otor Eff. Volumetric Eff. 53.4%

Pump (API: 25-150 R?B? 0-4)

Max Stroke Length 126.72 in Gas Free Plunger Stroke 67.71 in Gas Free Fillage 53.4% Gas Free Slippage 21 BBL/D Gas Free Displacement 110 BBL/D

Calculated Fluid Load Max 8909.3 lb Pump Fluid Load, Fo(Up-Dn) 6788 lb Damp Up 0.16018 Damp Dn 0.16018 Kг 91 lb/in Κt 1202 lb/in

Pump Intake Pressure 1200.4 psi (g) Pump HP 10.3 HP

Comments and Recommendations

45% RUNITIME, BEFORE BGC WAS INSTALLED

20 Oil BPD 30 Water BPD 50 Gas MCFD

- 886**6** f

Beam Loading 68.6% Stroke

SPM 7.32 spm Meas. Length 144.00 in Polished Rod

 Peak Load
 25043.2 lb

 Min Load
 11206.8 lb

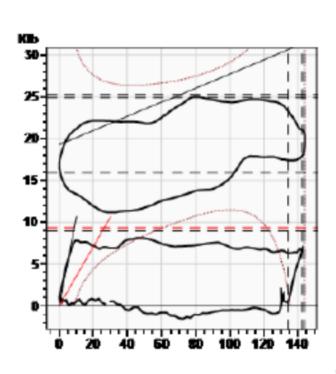
 Power
 23.5 HP

Case Study Number 6



Wellhead

Tubing Pressure 281.8 psi (g) Casing Pressure 20.6 psi (g)



Rod Loading

	Diameter (in)/ Length (ft)	Grade	Modified Goodman (05%)	Stress (lb)	Sensitivity (05%, H)
	125 22	FG	57 4%	20407.0	49.0%
	1 2650	D	74.9%	26288.4	617%
	0.875 1750	D	015%	28059.1	54.8%
	1£25 200	5B	25.8%	4787 8	11.1%
1	,				

Production oil *.* BBL/D

System Efficiencies

Polished Rod/Miotor Eff.

Pump.M otor Eff. Volumetric Eff.

94.3%

Pump (API: 25-150 R?B? 0-4)

 Max Stroke Length
 142.32 in

 Gas Free Plunger Stroke
 134.17 in

 Gas Free Fillage
 94.3%

 Gas Free Slippage
 23 BBL/D

 Gas Free Displacement
 235 BBL/D

Calculated Fluid Load Max 9357.0 lb Pump Fluid Load, Fo(Up-Dn) 7237 lb Damp Up 0.16018 Damp Dn 0.16018 Kr 91 lb/in Kt 1202 lb/in

Pump Intake Pressure 1199.8 psi (g) Pump HP 18.9 HP

Comments and Recommendations

90% RUN TIME. AFTER BGC WAS INSTALLED

45 Oil BPD 50 Water BPD 10 0 Gas MCFD

Analyzing Well Performance 98

Improving Oil and Gas Production with the Beam Mounted Gas Compressor Ali Al-Khatib, Mobil Oil Company, SPE.

A. L. Podio, University of Texas at Austin
J. N. McCoy, Doug Cook and Dieter Becker, Echometer Company